



# USED LUBE OIL REREFINING A SUCCESSFUL INVESTMENT

**Studi Tecnologie Progetti S.p.A.**  
*Engineering & Contractor*

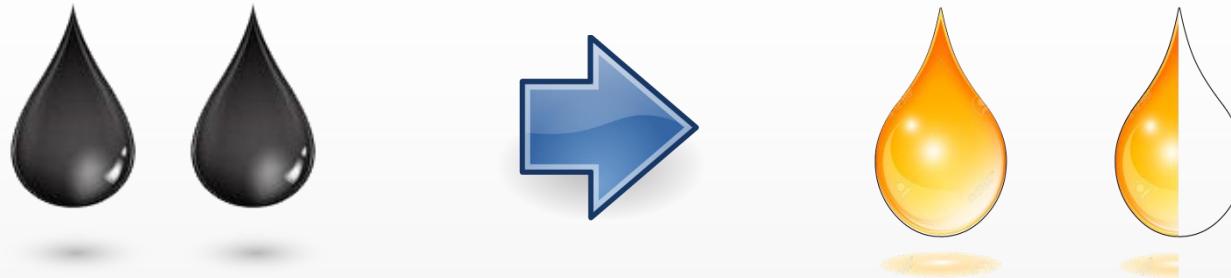
**Da Vinci Executive Center**  
**Viale Alexandre Gustave Eiffel 13/15 00148 Roma (RM), Italy**  
[www.stpitaly.eu](http://www.stpitaly.eu)

Used lube oil is a mixture of different types and grades of used lubricants, contaminants and degradation products coming from motor crankcases and industry.

Used lube oil is classified as toxic and hazardous waste to be properly disposed according to Waste Framework Directive 2008/98/EC and subject to the following requirements:

- Used lube oil shall be segregated and collected, not allowed to be dumped.
- Used lube oil shall be treated in accordance with waste hierarchy and protection of the environment and human health.
- Used lube oil treatments are established according to the level of contamination.

# 2 $\ell$ OF USED LUBE OIL GIVE 1,5 $\ell$ OF RE-REFINED OIL

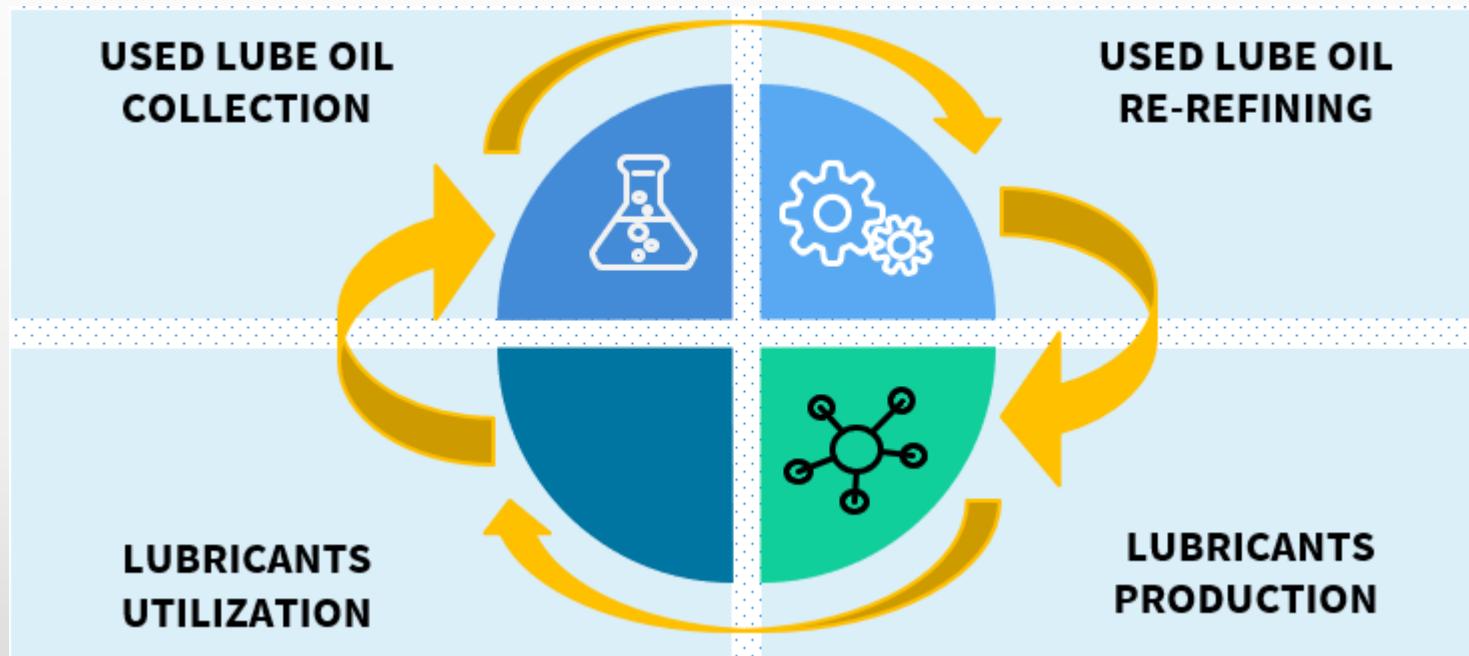


Re-refining of used lube oil is an economically attractive recycling method in terms of resources conservation and environment protection. It allows processing hazardous and toxic material in a safe and effective way to recover a high-quality oil product.

Used lube oil can be re-refined as many time as you like.

Used lube oil re-refining is a Circular Economy model and an attractive business opportunity as well as an environment protection process.

Lubrificants are ideal candidates for the circular economy because used lube oils retain much of their basic lubricating structure.



# USED LUBE OIL RE-REFINING ADVANTAGES



ENVIRONMENT PROTECTION



ENERGY CONSUMPTION OF RE-REFINING IS LOWER THAN FOR VIRGIN BASE OIL PRODUCTION



HIGH QUALITY PRODUCTS AND LESS DEPENDENCE ON IMPORTED OIL



**RE-REFINING IS A STRONG ECONOMIC INCENTIVE FOR ENVIRONMENT PROTECTION AND ENERGY SAVING**





Collection of used lube oil is the starting point for a successful Re-refining.

Re-refining depends on collection effectiveness and used lube oil availability.

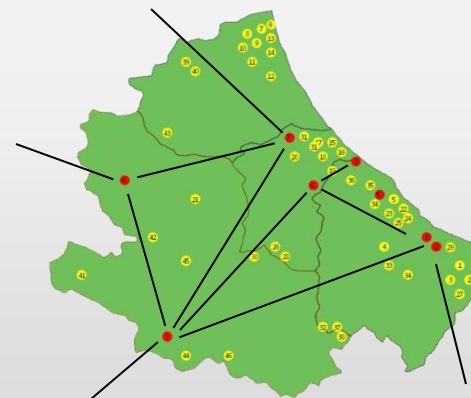
Used lube oil is collected at garages, maintenance/repair shops, gas stations, truck fleets and industries

Efficient collection facilities are a need for Re-refining in terms of used lube oil quantity and quality

**SUCCESS OF  
RE-REFINING  
DEPENDS ON THE  
COLLECTION SYSTEM**



- Investigation on used lube oil sources
- Division of the territory in Areas and Sectors
- Storage capacity of collection centres
- Transport network and truck drivers formation
- Used lube oil Pre-selection Tests
- Segregation of contaminants



# USED LUBE OIL PRESELECTION TESTS

- PCB / PCT, wt ppm 25 max
- Cl, wt % 0.5 max
- S, wt % 1.5 max
- Saponification N°, mgKOH/g 18 max
- Heavy fuel oil (drop test) pass
- Fatty acids (lux test) pass



Re-refining removes all the contaminants from used lube oil to recover base oil product.

During the last years many factors have obliged rerefiners to look for alternative Re-refining process, such as:

- increased use of additive packages in the formulation of lubricants and by consequence higher level of contaminants in the used oil
- increased amount of thermal degradation products due to longer mileage of the lubricants
- base oil product yield and specification

Among the available today processes, STP Re-refining offers a low energy high yield operation, high quality products and absence of noxious wastes or by products.



STP is **Pioneer** on Used Lube Oil Re-refining since 30 years to produce Base oils Group I and Group II, Marine Fuel RMB-30, VGO feedstock to Refinery Units.



STP has implemented several Re-refining Plants of different capacity worldwide and provides the latest high-tech green Re-refining Process.

# USED LUBE OIL RE-REFINING PLANT

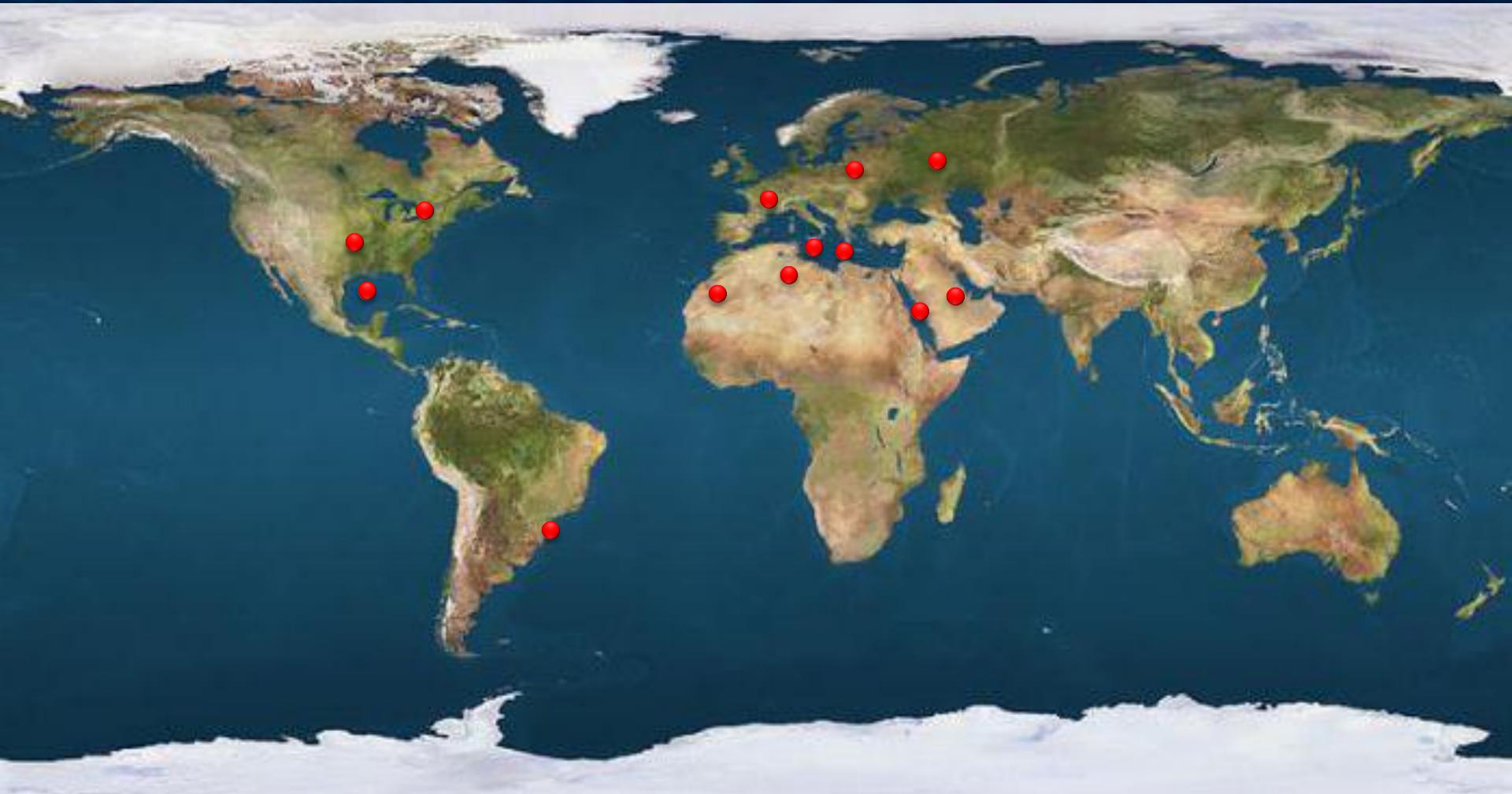
## STP LIST OF REFERENCES

Pos.	Client	Location	Capacity TPY	Year
1	YUNITCO	Yanbu, Saudi Arabia	190,000	Ongoing
2	HILL GROUP	Klaipeda, Lithuania	60,000	Ongoing
3	RE-GEN III	Oiltanking Galveston – Texas City, USA	5,600 BPSD	2022
4	ORIGIN INTL	Baltimore, USA	3,500 BPSD	2020
5	UNDISCLOSED	Puskhino, Russia	150,000	2019
6	AKWA	Mohammedia, Morocco	27,000	2017
7	KLOC KSCC	Ahmadi, Kuwait	33,000	2014
8	VEOLIA ES	St. Hyacinth, Canada	60,000	2013
9	ECOIL Italia	Ferrandina, Italy	65,000	2013
10	OSILUB (TOTAL/VEOLIA)	Gonfreville L'Orcher, France	120,000	2012
11	SIRAL SpA	Nola, Italy	30,000	2008
12	KLOC KSCC	Ahmadi, Kuwait	27,000	2000
13	SOTULUB	Bizerte, Tunisia	20,000	1998
14	GROUP LWART	Lençóis Paulista, Brazil	60,000	1997
15	RAMOIL	Naples, Italy	30,000	1996
16	SOTULUB	Bizerte, Tunisia	16,000	1989
17	LPC / CYCLON	Aspropyrgos, Greece	25,000	1985



# STP USED LUBE OIL RE-REFINING MAP

35+  
YEARS



API guidelines on Base Oil Quality Assurance and Base Oil Interchange classify base stocks into six **base stock groups** according to defined physical and chemical characteristics as follows:

## Group I

Base stocks containing less than 90 mass percent saturates and/or greater than 0.03 mass percent sulphur and having a viscosity index greater than or equal to 80 and less than 120.

## Group II

Base stocks containing greater than or equal to 90 mass percent saturates and less than or equal to 0.03 mass percent sulphur and having a viscosity index greater than or equal to 80 and less than 120.

## Group III

Base stocks containing greater than or equal to 90 mass percent saturates and less than or equal to 0.03 mass percent sulphur and having a viscosity index of greater than or equal to 120.

**Group IV**

Base stocks are polyalphaolefins (PAO)

**Group V**

All base stocks not included in Groups I, II, III, IV or VI.

**Group VI**

Base stocks are polyinternalolefins (PIO)

**Property**

Saturates Content  
Viscosity Index  
Sulphur Content

**Test Method**

ASTM D 2007  
ASTM D 2270  
ASTM D 2622, ASTM D 4294, ASTM D 4927, ASTM D 3120



STP Re-refining Process removes all the contaminants from the used lube oil and produce high quality base oil either API Group I or API Group I<sup>+</sup> and Group II.

STP Re-refining process does not release harmful or pollutant wastes to be disposed and is therefore environment friend.

Effluents are process water sent to treatment before disposal and off gas routed to thermal oxidizer to prevent smelling.

- Continuous plant operation
- High flexibility towards feedstock quality and composition
- High process yield. The lube oil recovery is more than 95% of the lubricant fraction present in the used oil.
- High separation selectivity, removal of contaminants and production of high-quality base oils
- Low energy and low utility consumption
- High on-stream efficiency without corrosion, fouling, coking
- Environment safeguarding operation and no use of acid and clays
- Management of all odorous compounds to eliminate malodorous and toxic emissions
- CAPEX and OPEX highly competitive



## 1. PRETREATMENT AND DEHYDRATION

Used oil is preheated to remove water, gasoline, VOC, light contaminants (solvents, glycols, lighter organic). Water and lights hydrocarbons are separated.

Lights hydrocarbons (gasoline) are used as substitution fuel.

## 2. LIGHT GASOIL STRIPPING

Dehydrated oil is stripped under vacuum for light gasoil removal and flash point adjustment of lube oil.

## 3. TFE VACUUM DISTILLATION

Oil from Light Gasoil stripper is sent to vacuum distillation to recover vacuum distillate oil fraction from heavier contaminants.

Vacuum distillation is carried out under high vacuum conditions, high temperature and by Thin film evaporator.

Thin film evaporator achieves high selectivity and oil purification from metals, heavy polymers, carbon, asphaltene and dust.

**Thin film evaporator (TFE)** is a vertical cylindrical shell enclosed in an heating jacket with an internal rotor distributing a thin layer of oil on the heated wall, by means of rotating blades.

By the action of rotor (electrically driven) high turbulence and back mixing occur in the thin layer of the oil film and product degradation at high temperature is avoided.

Main features of thin film evaporator are:

- short residence time in order of few seconds;
- high heat transfer rate through the film;
- efficient and regenerative cleaning of the contact surface

Cracking and fouling problems are avoided by keeping low residence time, low wall temperature and high flow turbulence.

Lube oil is recovered as distillate while heavy components, additives, metals and degradation products are concentrated in the bottom residue.

## ■ OPERATING PRINCIPLE

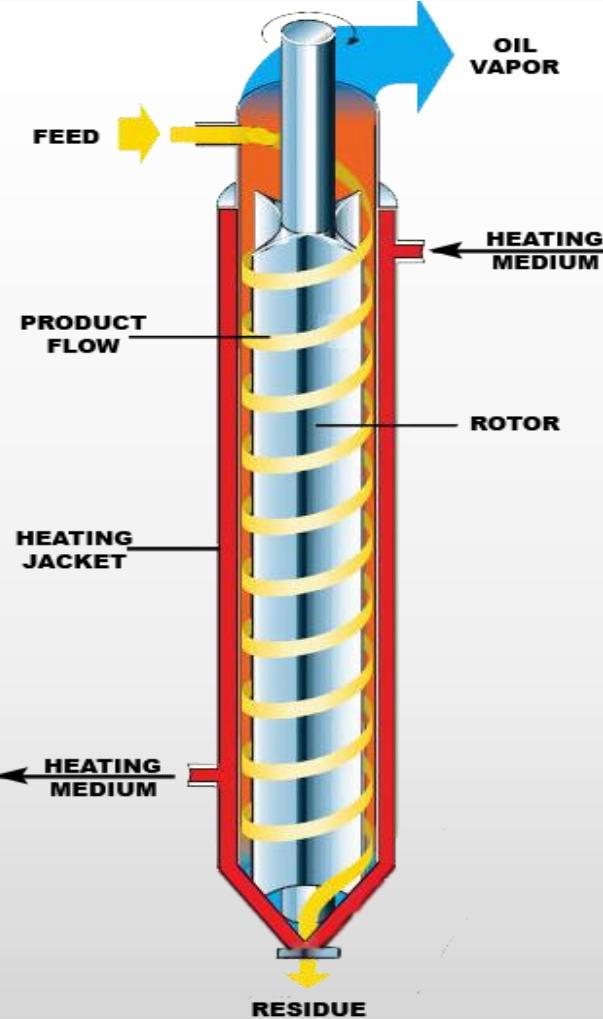
The Thin Film Evaporator consists of a cylindrical shell with internal rotor and external heating jacket

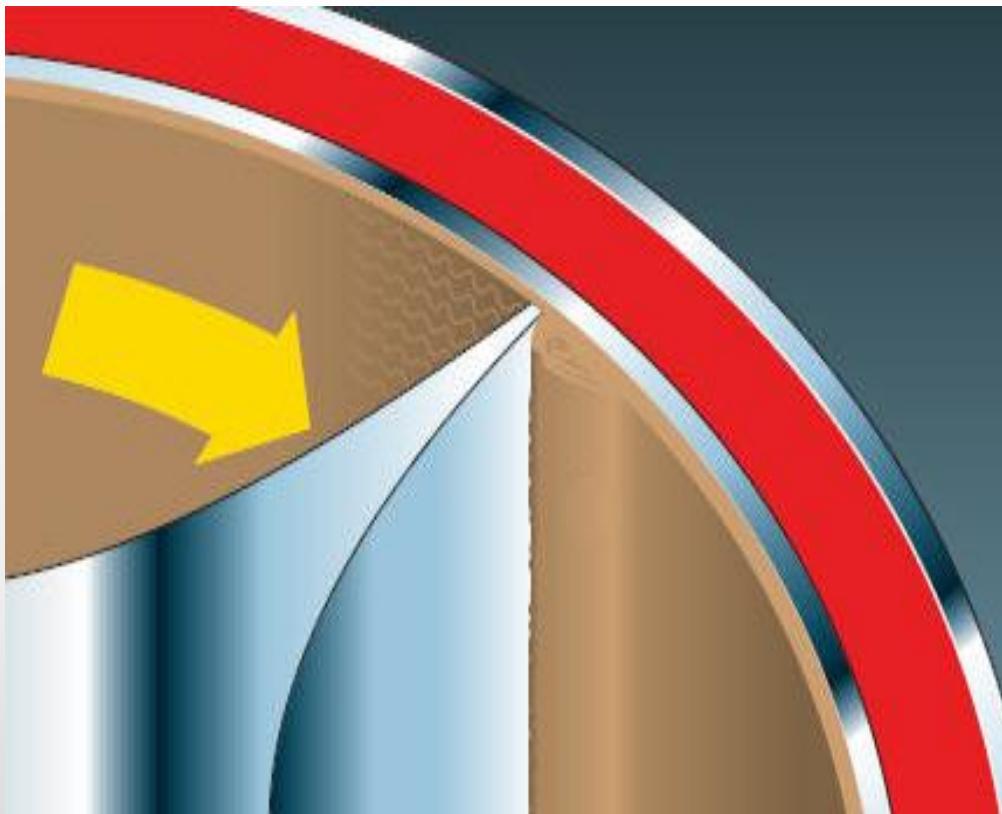
## ■ FEED

The feed is distributed by the rotor blades and spread on the heated wall to form a highly turbulent thin layer.

## ■ PRODUCTS

Oil fractions are evaporated and flow out up towards the top  
Heavy components flow in a spiral path down to the bottom as residue.





## FEATURES

- Short residence time and high turbulence in the film give high heat transfer coefficient and avoid overheating, cracking and fouling
- High evaporation rate is obtained by a simple pass
- High oil yield is achieved without degradation or polymerization of the oil
- High onstream factor and easy maintenance

#### 4. FINISHING AND FINAL FRACTIONATION

Distillate from Vacuum distillation is further finished to improve product quality. Finishing is done by Chemical Reactor to produce Base oil API Group I or by Hydrofinishing to produce Base oil API Group I<sup>+</sup> and API Group II.

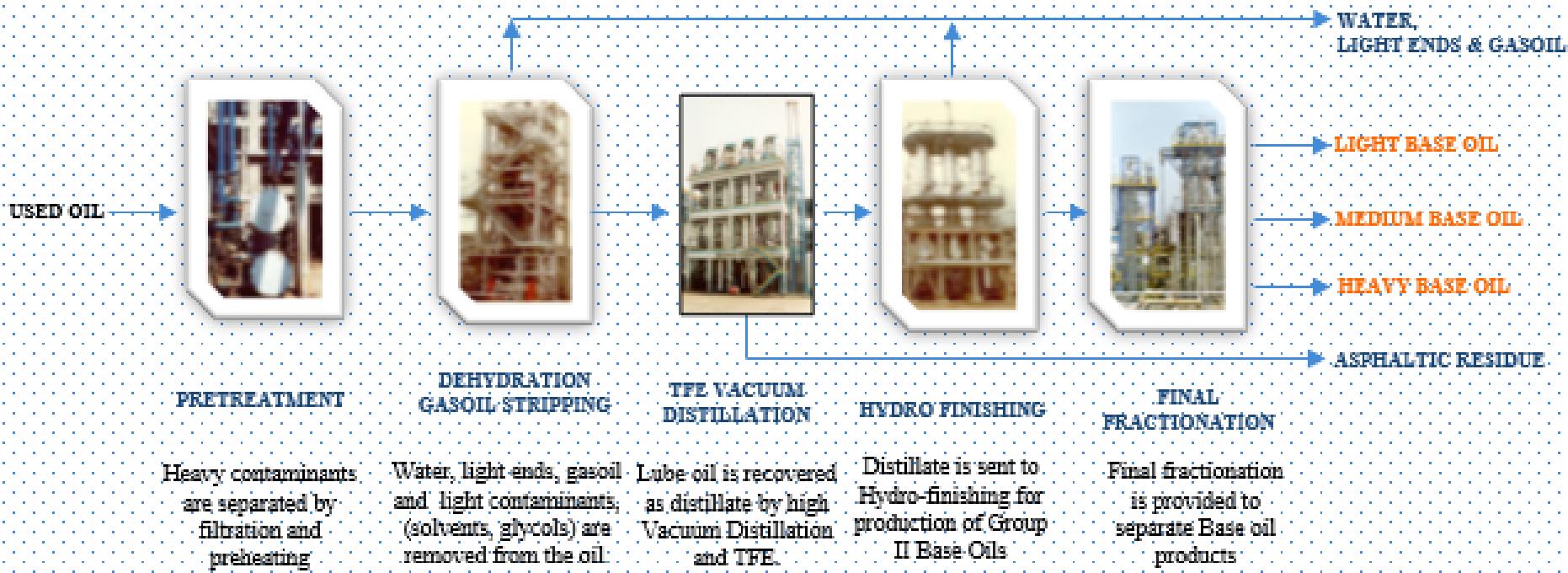
Hydrofinishing provides deep removal of contaminants such as chlorinated, sulfurous and oxygenated organic compounds and polyaromatic hydrocarbons and ensure oxydation and color stability.

Mild Hydrofinishing is used to produce Base oil API Group I<sup>+</sup>.

Severe Hydrofinishing is required to produce Base oils API Group II.

Finished oil is then fractionated to produce light, medium and heavy base oil.

## FLOW SCHEME



- ✓ Several Used Lube Oil Re-refining Plants implemented all over the world from 16,000 Ton/year to 270,000 Ton/year capacity
- ✓ Advanced vacuum system for high vacuum level stability, based on the combined use of steam ejectors and individual tubular condensers.
- ✓ High efficiency/low pressure drops structured packing in Vacuum distillation and Final fractionation, to reduce pressure drops and upgrade oil yield and product separation.
- ✓ Fixed blades Thin Film Evaporator (TFE) to avoid coking and fouling.
- ✓ Special type of API pumps and instrumentation for critical services.



- ✓ All pumps doubled to avoid plant shut down in case of pump failure.
- ✓ Full DCS/PLC plant automation for continuous operation.
- ✓ Indirect heating of heavy streams to prevent fouling.
- ✓ Special mechanical design for thermal flexibility, vacuum operation and fouling services.
- ✓ Use of antifouling to reduce maintenance and cleaning operation.
- ✓ Proprietary design of Base Oil finishing for Group I, Group I<sup>+</sup> and Group II

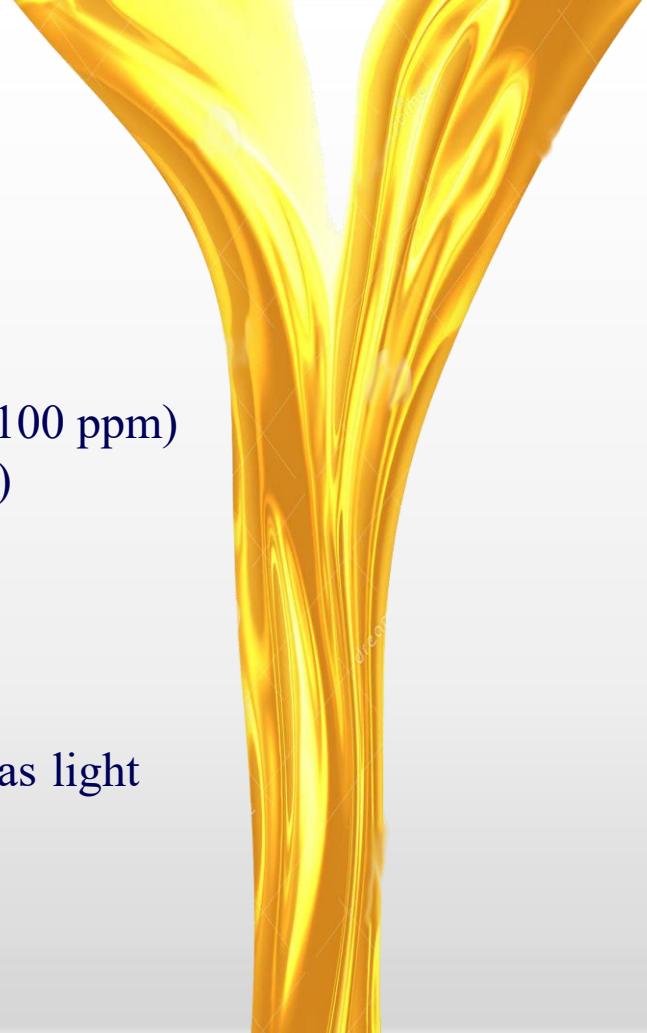


## LIGHT GASOIL

Specific gravity at 15 °C	0.850
End point, °C	370
Viscosity, cst at 40 °C	3-5
Sulfur, wt%	0.4 (after Hydrofinishing: 50 – 100 ppm)
Colour	2.5 (after Hydrofinishing: L 0.5)
Flash point, °C	80

Light Gasoil can be used as substitution fuel in the Plant or as light fuel oil in industrial fired heaters and/or boilers.

Light Gasoil after Hydrofinishing can be used as Diesel



**MARINE FUEL RMB-30 and VGO**

Distillation range, °C	370 - 550
Specific gravity at 15°C	0.900 max
Viscosity, cst @ 40°C	25-30
Flash point, °C	210 min
Sulfur, wt%	0.25
CCR, wt%	0.1 max
TAN, mgKOH/g	0.1 max
Ashes, wt%	0.2
Metals content, wt ppm	L 10



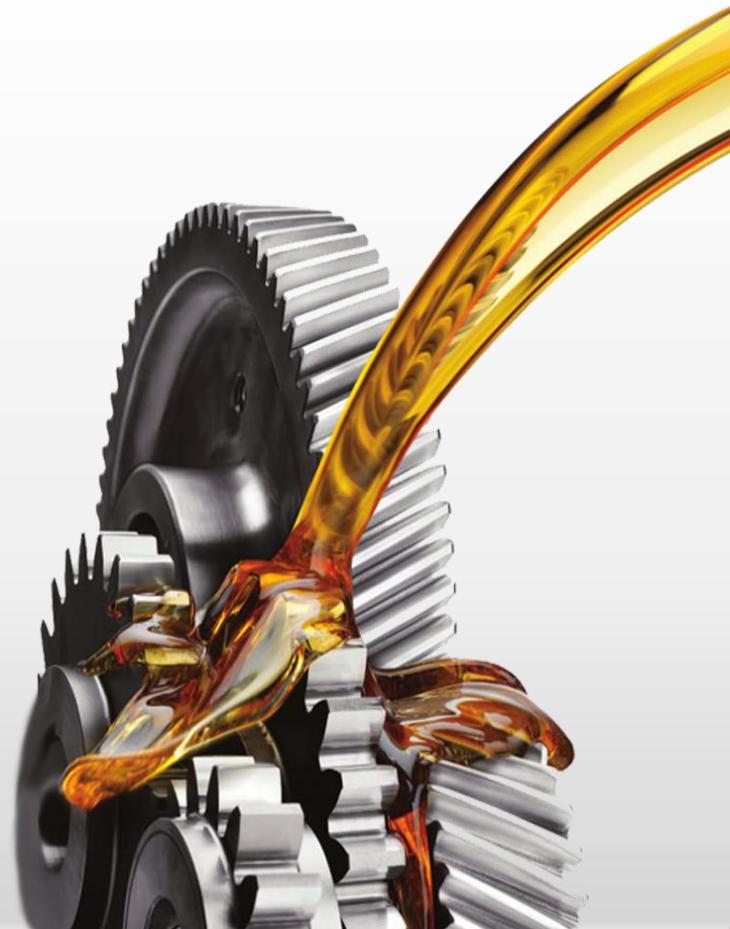
VGO is used as feedstock to Refinery FCC and HDC Units

### API GROUP I AND GROUP I<sup>+</sup>

Characteristics	Light Base Oil		Heavy Base Oil	
	Mild Hydrofinish Group I <sup>+</sup>	Chemical Treatment Group I	Mild Hydrofinish Group I <sup>+</sup>	Chemical Treatment Group I
Specific gravity at 15 °C	0.870	0.870	0.885	0.885
Viscosity, cst at 40 °C	25-32	25-32	85-95	85-95
Sulfur, wt%	0.05	0.25	0.05	0.30
CCR, wt%	L 0.01	0.05	L 0.01	0.07
Colour	L 1.0	2.0	L 1.5	2.5
TAN, mg KOH/g	L 0.01	0.03	L 0.01	0.05
Flash point, °C	220	220	260	260
Pour point, °C	-3	-3	-6	-6
Metals, ppm	absent	L 10	absent	L 10

### API GROUP II

Characteristics	Light Base Oil	Heavy Base Oil
Specific gravity at 15 °C	0.870	0.880
Viscosity, cst at 40 °C	25-32	85-95
Viscosity Index	110	115
Sulfur, wt%	L 0.03	L 0.03
Saturates, wt%	≥90	≥90
CCR, wt%	L 0.01	L 0.01
Colour	L 0.5	L 1.0
TAN, mg KOH/g	L 0.01	L 0.01
Flash point, °C	220	260
Pour point, °C	-6	-9
Metals, ppm	absent	absent

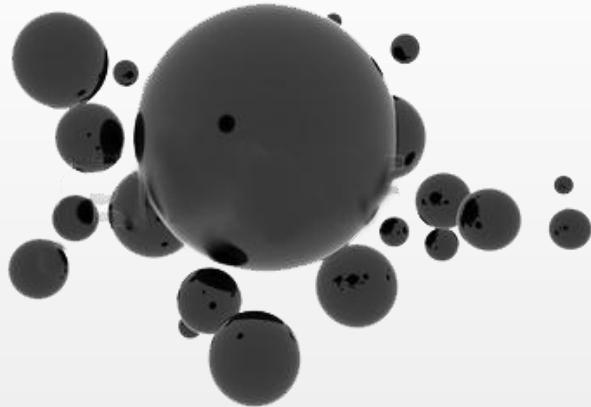


## API GROUP II

Characteristics	Light Base Oil	Heavy Base Oil
PCB, wt ppm	L 1	L 1
PCT, wt ppm	L 5	L 5
PNA, wt ppm	L 1000	L 1000
Cl, wt ppm	L 1	L 1
Cu corrosion	1a	1a
Noack , %wt	10	L 5
Saponification N°	L 0.5	L 0.5
Demulsification N°	10	10
Oxydation stability		
CCR increase, %	0.10	0.15
Viscosity ratio @ 40°C	1.09	1.1
Color stability	1.0	1.0



## ASPHALTIC RESIDUE



Specific gravity at 15 °C 0.950 - 1.050

Viscosity, cst  
at 40 °C 10,000  
at 100 °C 80

Sulfated ash, wt% 3-4

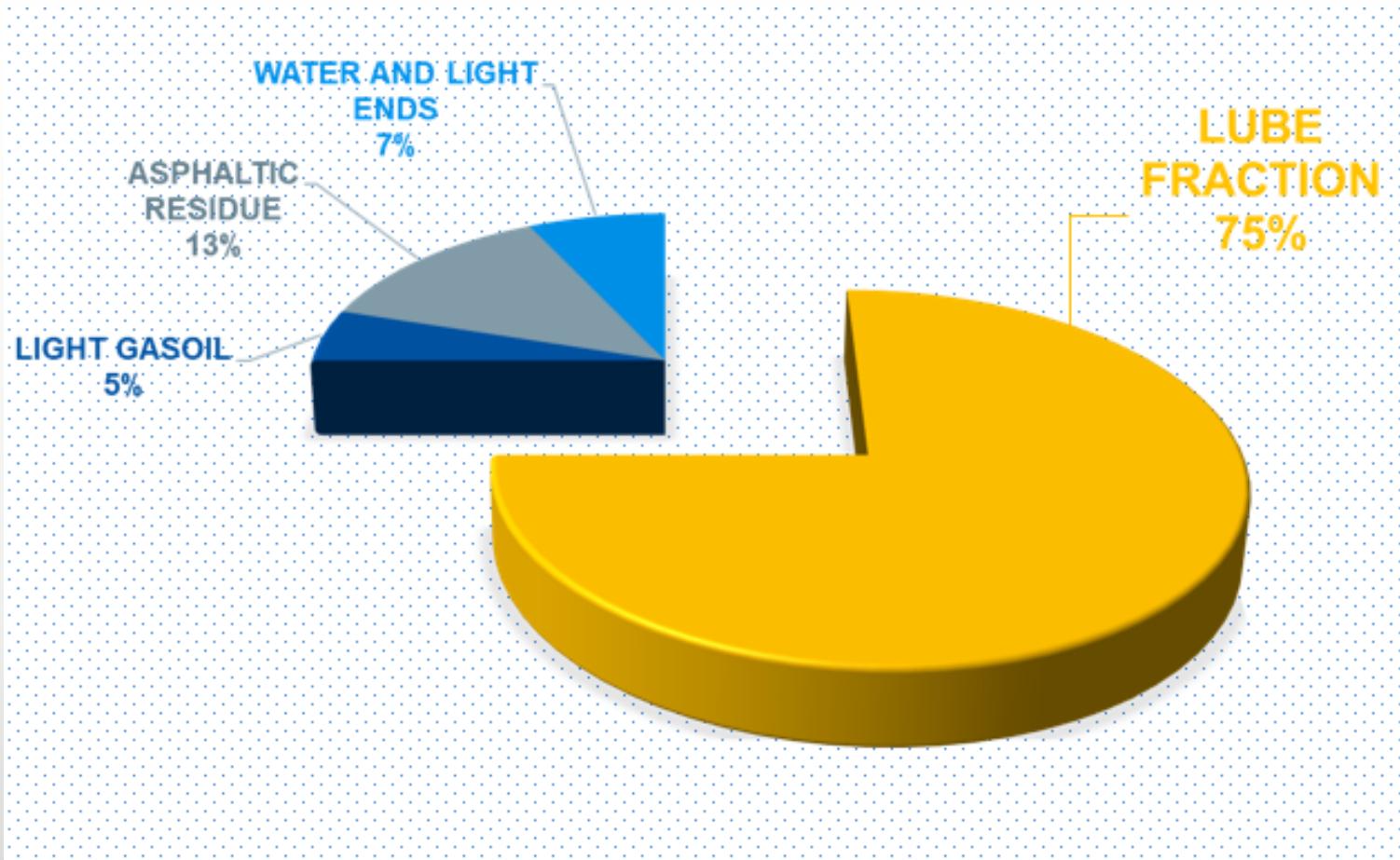
Sulfur, wt% 1-2

Penetration, mm/10 at 25 °C 200-400

Softening point, °C 15-20

Residue contains high quantity of asphaltenes, polymers, metals and can be used for the production of paving asphalt, bituminous protective coating, asphalt blending or as fuel in the cement factories.

## USED LUBE OIL COMPOSITION



- Electric power system
- Steam system
- Cooling water system
- Compressed air system
- Waste Water Treatment
- Thermal Oil System
- Thermal Oxidizer
- Hydrogen Plant (in case of Group I<sup>+</sup>, II)
- Flare system (in case of Group I<sup>+</sup>, II)
- Fire fighting system
- Used oil and Products storage and loading system



Service	Base oil API Group I Production	Base oil API Group II Production
Electric power, Kwh	25	55
Circulating cooling water, m <sup>3</sup>	30	40
Steam, Kg	340	400
Circulating Thermal Oil, 10 <sup>3</sup> Kcal	130	320

Operating labour requirements is depending on Plant operating philosophy, site location and Plant implementation within an existing complex.

Typical labor and technical staff requirement of the Re-refining Unit is as follows:

▪ Plant Manager	1
Plant Operation:	
▪ Supervisor/Board person (1 per shift)	4
▪ Operators (2 per shift)	8
Maintenance/Workshop	
▪ Supervisors	1
▪ Workers	4
▪ Laboratory	2
<hr/>	
<b>Total</b>	<b>20</b>



The staffing estimate is provided as a guideline and is intended for preliminary assessment.

The Used Oil Re-refining Unit is a very compact facility.

Typical ISBL layout area required for a 50,000 MTPY Re-refining Unit is as follows :

Production of Base Oil API Group I  
(without Hydrofinishing)

**2,000 sq.mt**

Production of Base Oil API Group I<sup>+</sup> and II  
(including Hydrofinishing and H2 Plant))

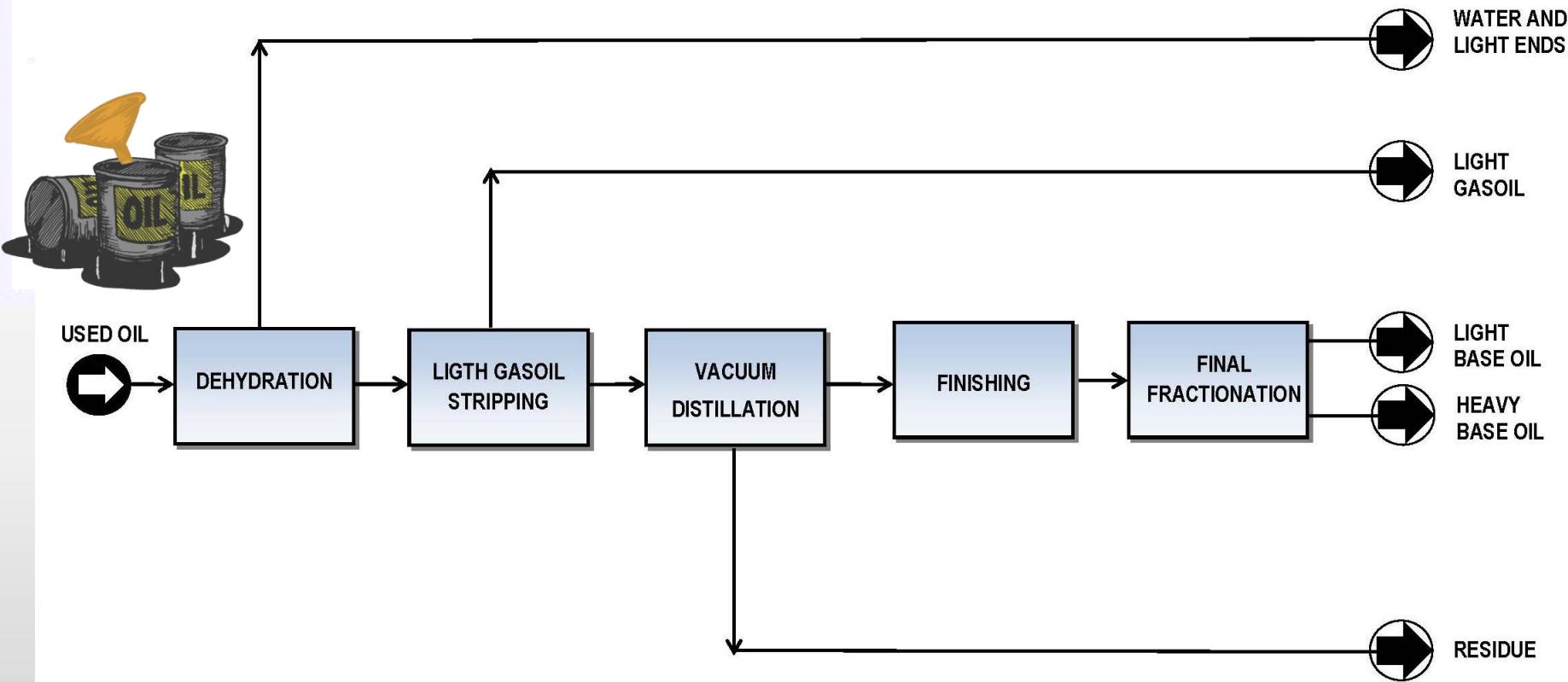
**10,000 sq.mt**



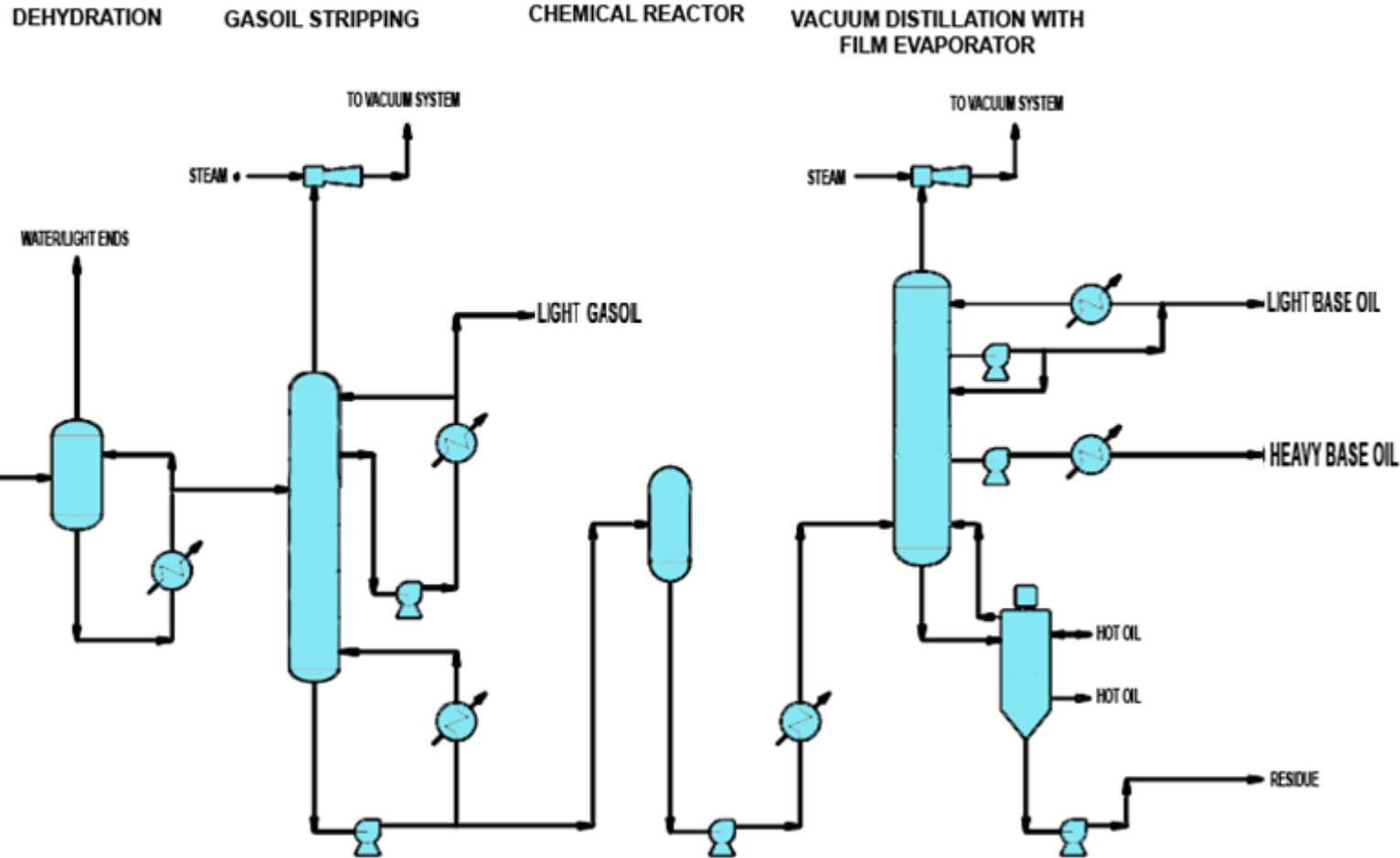
## FLOW SCHEMES

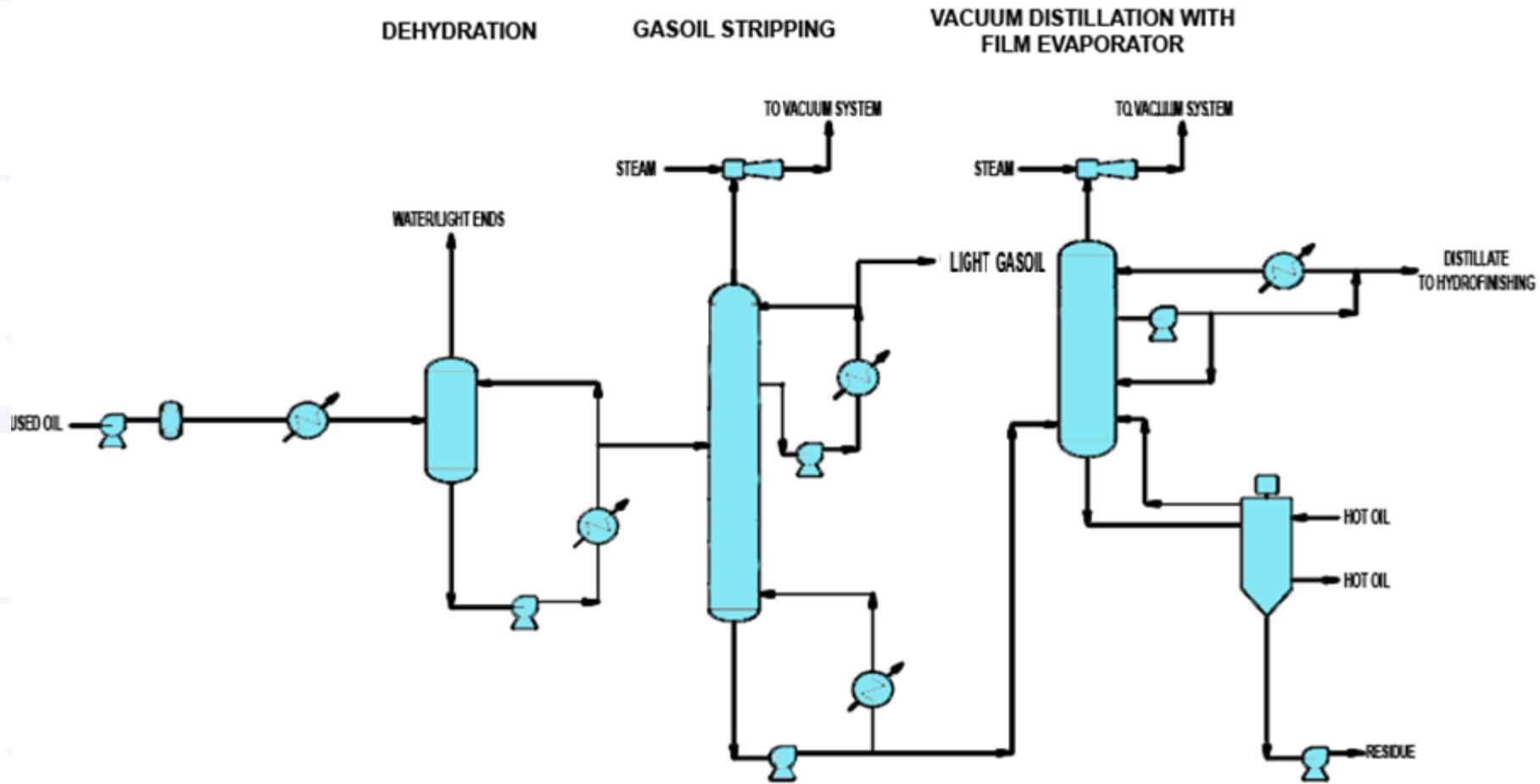


# BLOCK SCHEME

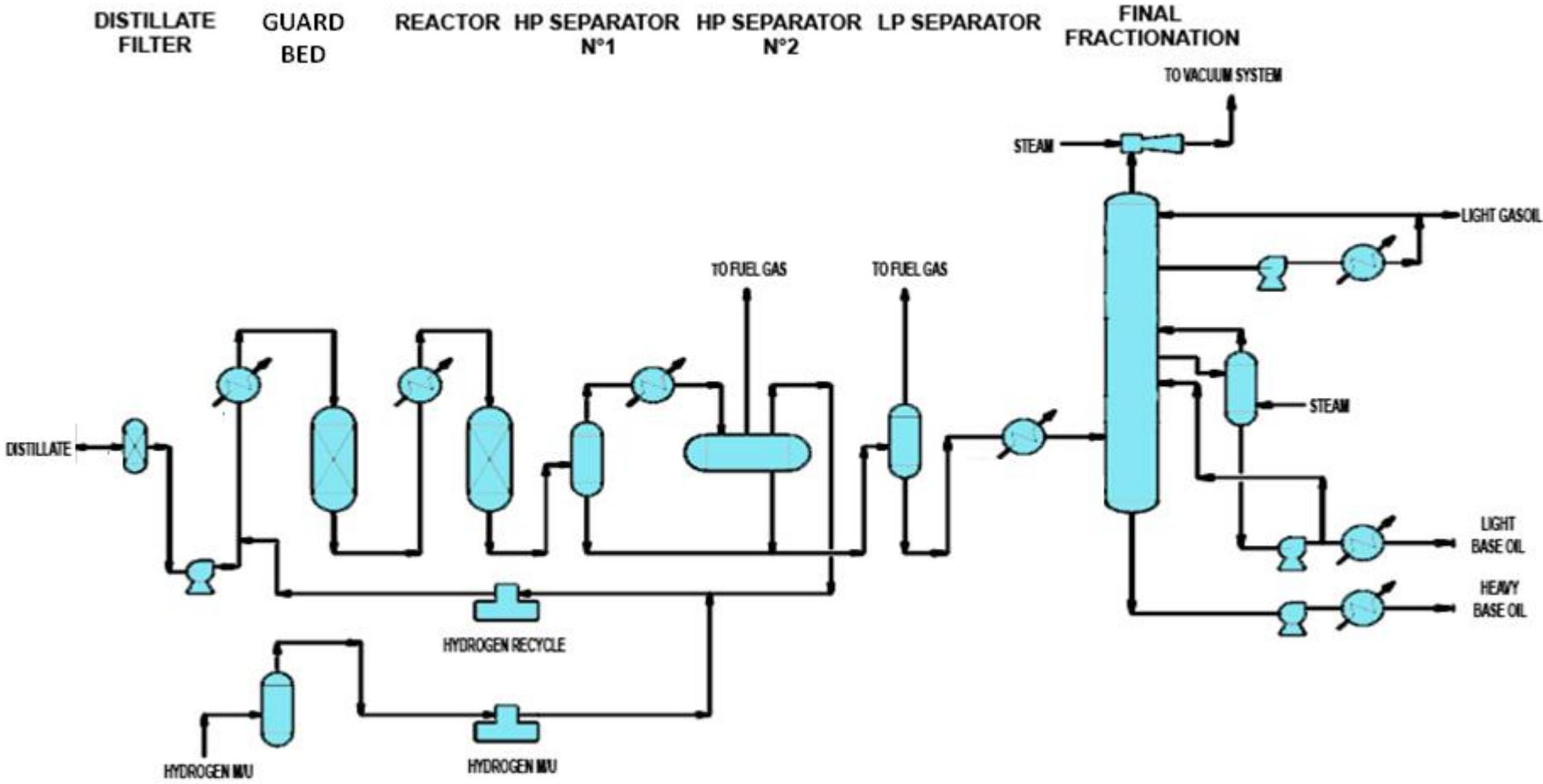


# PRODUCTION OF BASE OIL GROUP I





# PRODUCTION OF BASE OIL API GROUP II AND API GROUP I+



# CLIENT: YUNITCO

35+  
YEARS



**Client: YUNITCO**  
Yambu, Saudi ARABIA

**Capacity: 190,000 Ton/year**

**Year: Ongoing**



**Client: HILL GROUP**  
Klaipeda, Lithuania

**Capacity: 60,000 Ton/year**

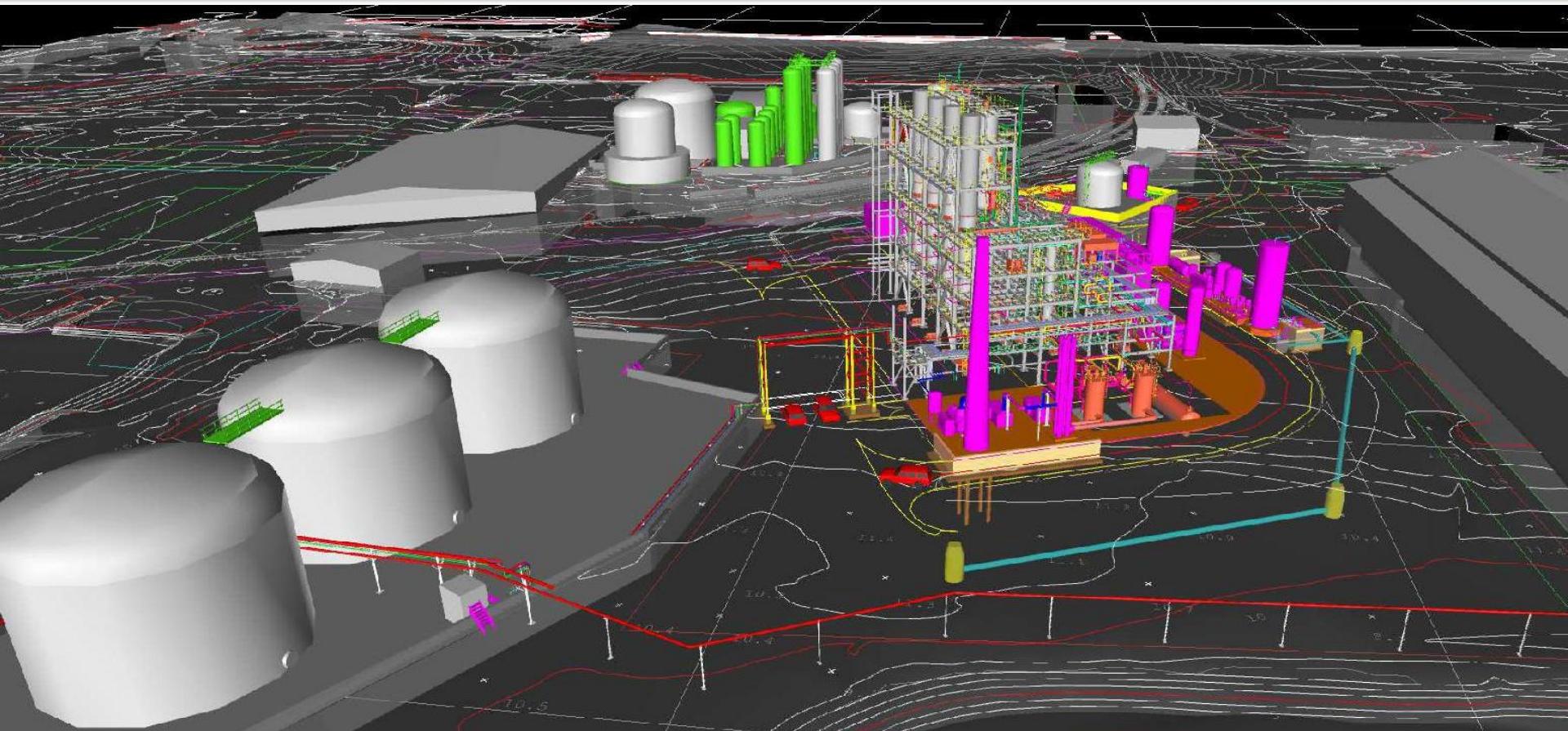
**Year: Ongoing**



**Client: ReGen III**  
Galveston Texas City, USA

**Capacity: 5,600 BPSD**  
( 270,000 Ton/y )

**Year: 2022**



**Client:** ORIGIN INTL  
Baltimore, USA

**Capacity:** 3,500 BPSD

**Year:** 2020



**Client: UNDISCLOSED**  
Russia

**Capacity: 150,000 Ton/year**

**Year: 2019**

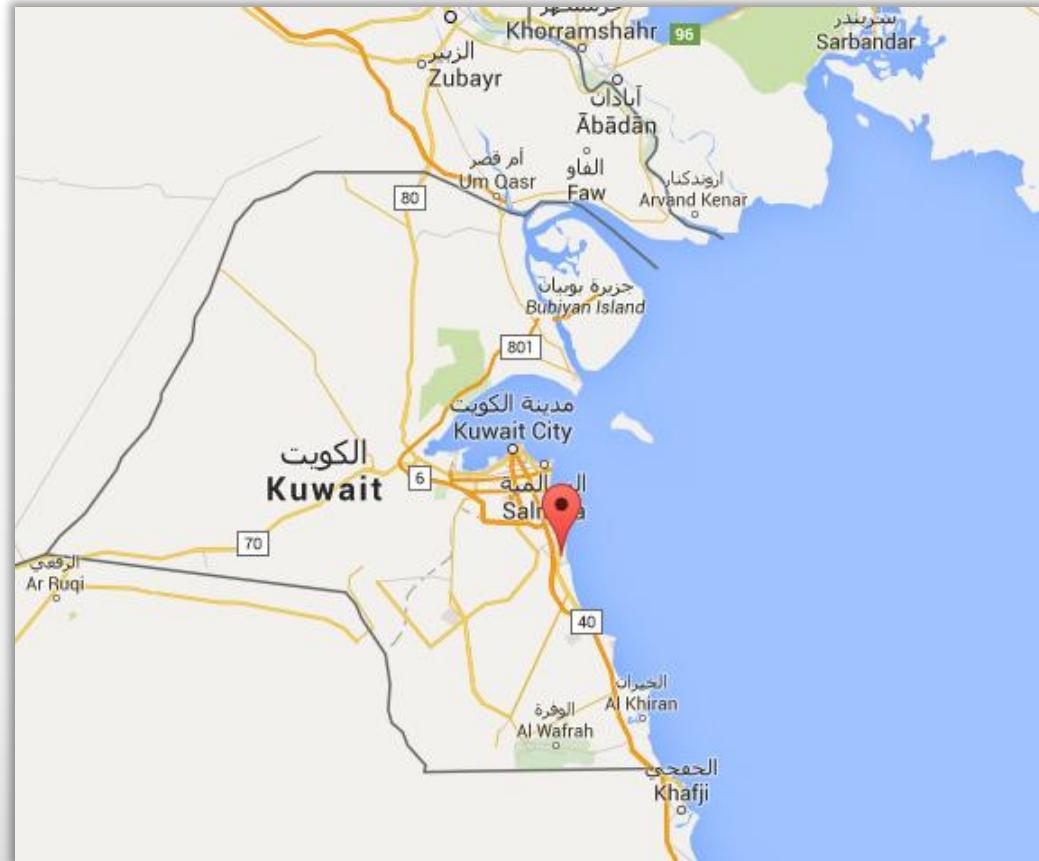
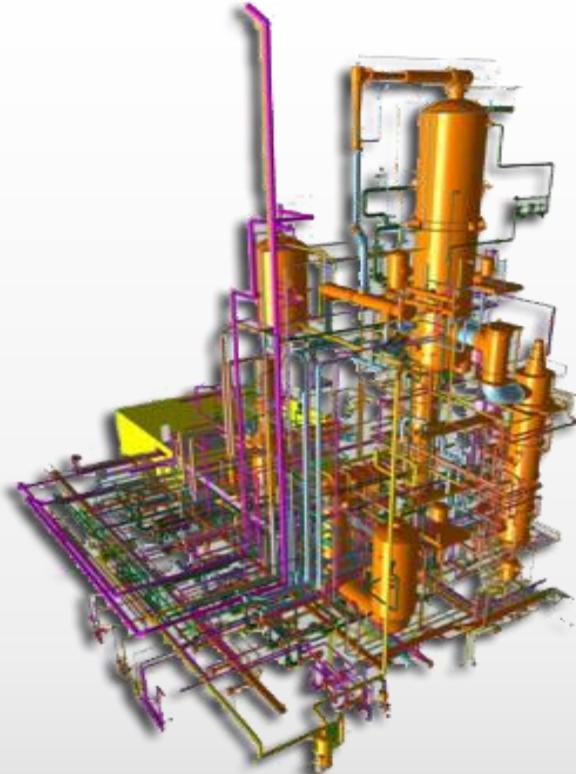


**Client: UNDISCLOSED**  
Russia

**Capacity: 150,000 Ton/year**

**Year: 2019**

## REFERENCE PLANT: KLOC



**Client:** KLOC KSCC  
Ahmadi, Kuwait

**Capacity:** 33,000 Ton/year  
(Revamping)

**Year:** 2014



**Client:** VEOLIA ES CANADA  
St. Hyacinthe, Quebec

**Capacity:** 60,000 Ton/year

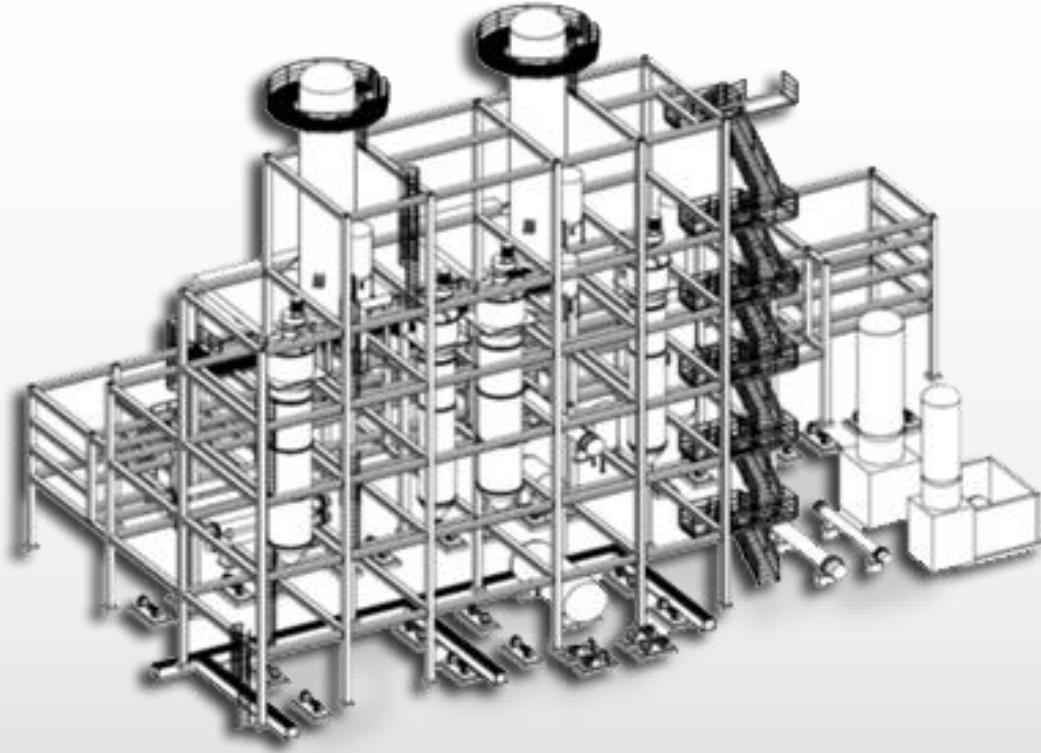
**Year:** 2013



**Client:** VEOLIA ES CANADA  
St. Hyacinthe, Quebec

**Capacity:** 60,000 Ton/year

**Year:** 2013



**Client:** ECOIL ITALIA  
Ferrandina, Italy

**Capacity:** 65,000 Ton/year

**Year:** 2013

# REFERENCE PLANT: OSILUB



**Client: TOTAL / VEOLIA – OSILUB**  
Gonfreville L'Orcher – France

**Capacity: 120,000 Ton/year**

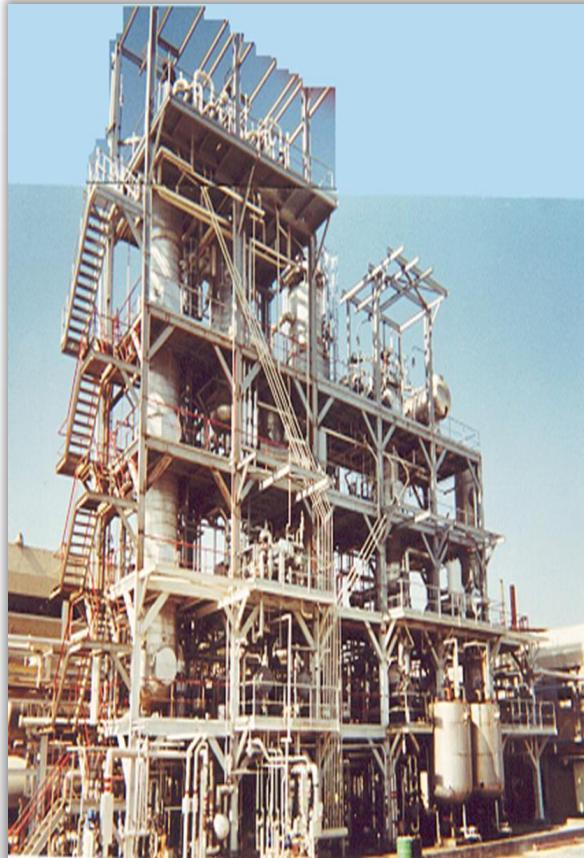
**Year: 2012**



**Client: SIRAL SpA**  
**Nola, Italy**

**Capacity: 30,000 ton/year**

**Year: 2008**



**Client:** KLOC Kuwait Lube Oil Company  
Ahmadi, Kuwait

**Capacity:** 27,000 Ton/year

**Year:** 2000



**Client:** SOTULUB Société Tunisienne Lubrifiants  
Bizerte, Tunisia

**Capacity:** 20,000 Ton/year

**Year:** 1998



**Client:** GRUPO LWART  
Lencois Paulista, Brazil

**Capacity:** 60,000 Ton/year

**Year:** 1997



**Client:** RAMOIL  
Naples, Italy

**Capacity:** 30,000 Ton/year

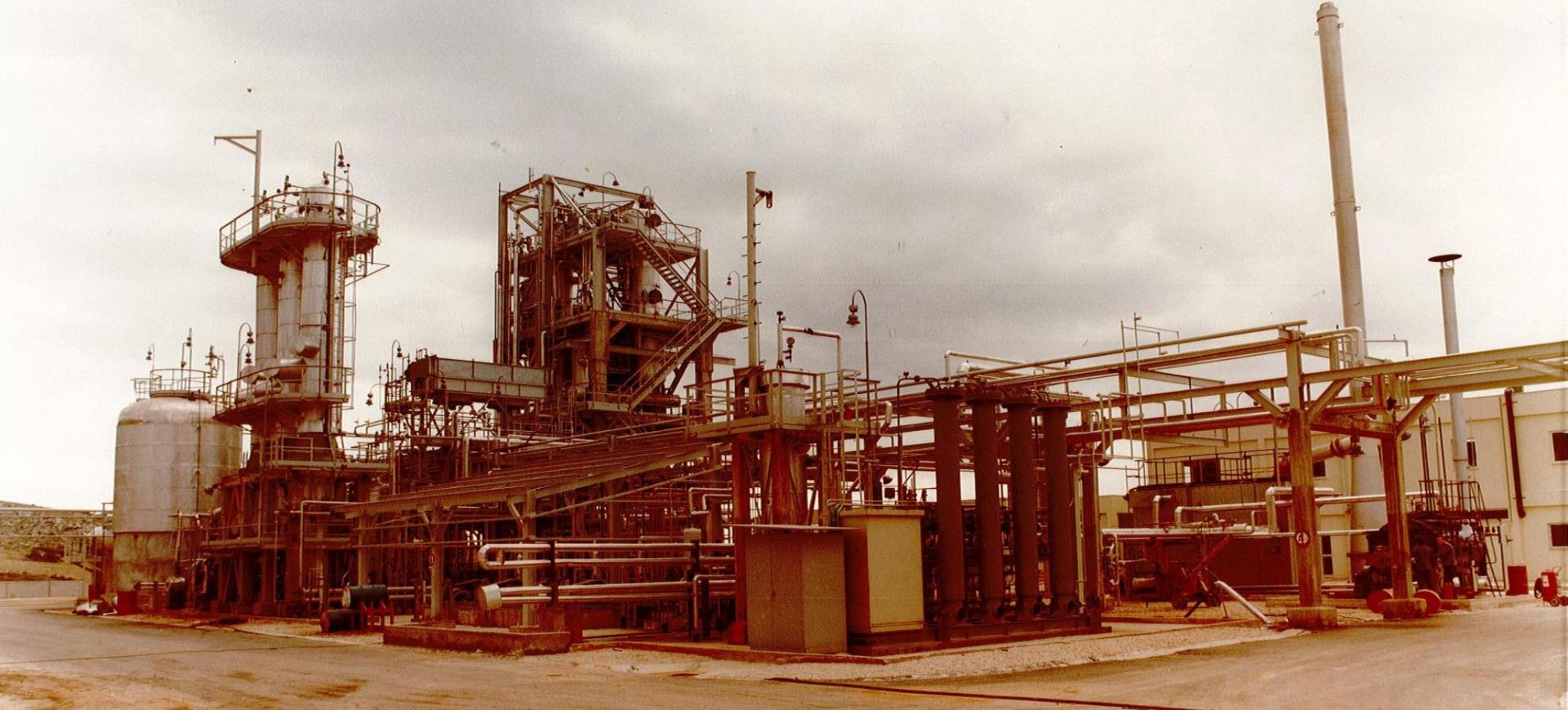
**Year:** 1996



**Client:** SOTULUB Société Tunisienne Lubrifiants  
Bizerte Tunisie

**Capacity:** 16,000 Ton/year

**Year:** 1989



**Client:** LPC/CYCLON Hellas  
Aspropyrgos, Greece

**Capacity:** 25,000 Ton/year

**Year:** 1985

## STP Publications and Conference presentations on Used Lube Oil Re-refining:

- *A Project case: the 120,000 Ton/year OSILUB Re-refining Plant*, 3<sup>rd</sup> CIS Base Oils, Lubrificants & Fuels Annual Conference, Moscow, Russia, May 2015.
- *A successful waste management investment*, UNEP-BIMTECH International Expert's Workshop on Destruction Technologies for Waste Oils, New Delhi, India, November 2011.
- *A re-refining eco-friendly technology*, Indian Institute of Petroleum (IIP) Workshop on Used Oil Recycling, Dehradun, India, November 1999.
- *Modification of existing re-refining units and realization of new modular units*, NORA Conference and Trade Show, Palm Springs, USA, November 1999
- *The hidden asset*, Fifth Conference on Spent Lube Oil Re-refining, Las Vegas, USA, September 1982.
- *The used lube oil: a resource not to underevaluate*, Chemical Industries Magazine, Italy, February 1982.



# USED LUBE OIL RE-REFINING

35+  
YEARS

## TESTIMONIALS



## ORIGIN INTERNATIONAL INC COMMENCES BALTIMORE RECYCLING PLANT PROJECT

October 28, 2019 09:03 AM Eastern Daylight Time

### CONTACTS



Rachel Deaver  
Public  
Relations  
443-573-1042  
[rd@origin-americas.us](mailto:rd@origin-americas.us)

BALTIMORE--(BUSINESS WIRE)--Origin International Inc ("Origin") is proceeding with the next phase of development for the United States East Coast's largest and only water bounded used oil recycling plant.

Origin is a leading environmental infrastructure and services group operating in the United States and Europe. To date Origin has established itself as one of the largest privately held used oil collectors in the United States as well as the largest mobile hydrocarbon recovery service provider in Europe which includes degassing, filtration and vapor recovery for maritime vessels, tank farms and industrial facilities.

Origin's planned construction project in its Baltimore terminal will provide the United States East Coast with its largest, most versatile and only water bounded used oil recycling plant, regenerating close to one million barrels per annum of used and contaminated liquid hydrocarbons that it can receive by truck, rail, vessel or barge. The new plant will create an estimated 200 jobs during peak construction and 20 new full-time jobs at the site, with recruitment focused on residents in the Baltimore area.

The engineering and construction management team is making progress on several fronts. Day & Zimmermann Process & Industrial division is providing overall project management services as well as engineering and procurement for offsites and utilities equipment. WBCM Construction Services with sister company Whitney Bailey Cox & Magnani LLC is performing overall construction management, preconstruction planning and permitting services. Studi Tecnologie Progetti S.p.A. Italy (STP) is performing process unit engineering, detailed design, procurement and site supervision. Becht Engineering is serving as owner's engineer for the entire project. Front-end engineering and design has been completed by STP for the process unit and is in progress for offsites and utilities. Detailed design, preconstruction site planning and permitting are underway.

"This project represents a major milestone in Origin's strategic growth plan in terms of vertical integration as well as providing a cradle to grave solution for the broadest range of waste liquid hydrocarbons. Our goal is that this plant will provide significant environmental and community related benefits to the city of Baltimore and surrounding mid-Atlantic regions," said Nicholas Myerson, CEO of Origin.

"Day & Zimmermann is excited to be part of Origin's strategic growth plan," says Bill Wasilewski, President of Day & Zimmermann's Process & Industrial Division. "We are particularly pleased to work within the capital project delivery team that has a common focus on delivering an asset that maximizes its return to investors."

#### About Origin International

Origin International seeks to acquire and consolidate strategically located oil terminals, oil processing facilities, and storage assets throughout North America and Europe. The firm's acquisition strategy focuses on waste oil recovery and recycling segments. For more information about Origin, visit [www.origin-international.us](http://www.origin-international.us). For more information on Origin's largest shareholder, Element Group SA, visit [www.element-alpha.com](http://www.element-alpha.com).



CERTIFICATE OF

## APPRECIATION



*This certificate is awarded to*

**MR. ALESSIO BIANCARI**

*for his contributions as a*

**SPEAKER**

*at the*

**7<sup>th</sup> Annual Base Oils & Lubricants Conference 2019**

**21-23 May 2019**

*Radisson Collection Hotel*

*Moscow, Russian Federation*



**ARLANXEO**  
Performance Elastomers



**EVONIK**  
POWER TO CREATE



CEO, GLOBUC



**ExxonMobil**



**CIS BASE OILS,  
LUBRICANTS & FUELS**  
III Annual Conference

**26 - 28 May 2015  
Moscow, Russia**

## 13:30 III USED OILS RE-REFINING TECHNOLOGIES

- Overview of used oils collection and re-refining projects in Russia and the CIS

**VLADIMIR SPIRKIN**, *Professor, Academician, GUBKIN RUSSIAN STATE UNIVERSITY OF OIL AND GAS*

- Used oil and oil sludge recycling

**BORISS NIGROVSKY**, *Sales Manager CIS, FLUID SOLUTIONS*

- Waste oil treatment. A question of strategy

**LUIS BERTRAND**, *Vice President, SWEET GAZOIL*

- STP project in France: The OSILUB plant is one of the largest re-refining plant in the world

**CARLO GUSTAVO LOMBARDI**, *CEO / Managing Director, S.T.P. STUDI TECNOLOGIE PROGETTI*

# PARTICIPATION TO UNITED NATIONS ENVIRONMENT PROGRAMME



UNITED NATIONS ENVIRONMENT PROGRAMME  
Programme des Nations Unies pour l'Environnement  
Programa de las Naciones Unidas para el Medio Ambiente  
Espace pour l'Environnement  
Oficinas de las Naciones Unidas para el Medio Ambiente  
البيئة  
聯合國環境署



Our ref: 65

11 November 2011

Dear Mr. Lombardi,

I am pleased to advise that UNEP's International Environmental Technology Centre has undertaken a project to develop a Compendium of Destruction Technologies for waste oils. The compendium will include both technologies for waste oil recycling as well as destruction technologies for non-recyclable oils through converting it into fuel and/or incinerating it. The objective is to assist developing countries with information on destruction technologies and to enable them to assess different technologies in order to select the one suitable for their local conditions.

We are working with Birla Institute of Management and Technology, India, on this project. Apart from the Compendium, we will also develop interactive software to facilitate the technology selection process. A draft version of the compendium and the interactive software will soon be ready.

In order to enrich the work with the knowledge and inputs from international experts, we are organizing an International Experts Workshop in New Delhi, India, from 30 November to 2 December 2011. Noting your expertise and experience in the field of waste management, we would like to invite you as an expert to the workshop and request you to provide your valuable inputs. Please confirm your attendance to Mr. Surya Prakash Chaudhary, Senior Programme Officer, Email: [surya.chaudhary@unep.org](mailto:surya.chaudhary@unep.org) with copy to Ms. Kanako Uwasu, Programme Assistant, Email: [kanako.uwasu@unep.org](mailto:kanako.uwasu@unep.org).

The detailed agenda of the Workshop is attached. The venue of the workshop will be Hotel Clarion Collection (formerly Qutab Hotel) Unit of Edgewater Hotels Pvt. Ltd. Shahbad Jat Singh Marg, New Delhi 110016. Upon receiving your confirmation, we will send you the draft compendium which will be discussed in the meeting.

In the light of STP's status as a large multinational company, we look forward to your early confirmation and participation in the workshop.

Sincerely yours,

Matthew Gubb  
Director

Mr. Carlo Gustavo Lombardi  
CEO/Managing Director  
STP Studi Tecnologie Progetti S.r.l.  
Piazzale Ezio Tassanelli, 97  
00144 - Roma, Italy  
E-mail: [cglobardi@stpitaly.eu](mailto:cglobardi@stpitaly.eu)

Attachment: Agenda of the workshop

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Division of Technology, Industry and Economics:  
International Environmental Technology Centre (IETC)  
2-110, Ryokuchi-koen, Tsurumi-ku, Osaka 538-0096, Japan, Tel: +81.6.6915.4581; Fax: +81.6.6915.0304  
E-mail: [ietc@unep.org](mailto:ietc@unep.org); URL: <http://www.unep.org/ietc>



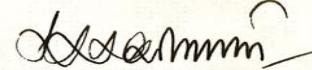
UNITED NATIONS ENVIRONMENT PROGRAMME  
UNEP-DTIE-IETC

In collaboration with  
Birla Institute of Management Technology (BIMTECH)

**International Experts' Workshop on  
Destruction Technologies for Waste Oils**

*Certificate of Participation*

This is to certify that Mr./Ms. Carlo Gustavo Lombardo has participated in International Workshop of experts for reviewing the draft manuscript of "Destruction Technologies for Waste Oils" held in New Delhi – India, during 30th Nov. 2011 to 2nd December 2011 in India, and has contributed in modifying the document. The workshop was organized by the United Nations Environment Programme UNEP-DTIE-IETC in collaboration with Birla Institute of Management Technology, Greater Noida – India.



Dr. H. Chaturvedi  
Director, BIMTECH

# STP ATTENDANCE TO NORA CONFERENCE AT PALM SPRINGS (USA)



## National Oil Recyclers Association

12429 Cedar Road • Suite 26 • Cleveland, Ohio 44106-3172 • (216)791-7316 • Fax (216)791-6047  
Kathryn McWilliams - Executive Director  
E-Mail Address: [NatOilRA@aol.com](mailto:NatOilRA@aol.com)  
[www.noraoil.com](http://www.noraoil.com)

February 7, 2000

Carlo Lombardi  
STP Studi Tecnici Procedure  
Via D Snaotta 100  
Rome, Italy 00147

Dear Lombardi:

The National Oil Recyclers Association's 1999 Conference and Trade Show in Palm Springs was a success in part because of fine presentations such as yours. Each Conference we orchestrate is built on the efforts of many individuals and I'd like you to know that your contribution was appreciated.

The Conference was well attended with over 300 people taking part in the meetings, presentations and activities. And, indications are that your presentation was received quite well.

On behalf of the Conference Planning Committee, the attendees and myself, thank you for your participation. We hope you had an enjoyable experience and trust you will consider submitting a presentation proposal for the 2000 Conference.

Sincerely,

Teresa S. Molnar  
Program Coordinator

/ter



## 1999 LIQUID RECYCLING CONFERENCE AND TRADE SHOW PALM SPRINGS – November 10 – 13, 1999

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### MODIFICATION OF EXISTING REREFINING UNITS AND REALIZATION OF NEW MODULAR UNITS

Mr. Carlo G. Lombardi  
Chief Executive Officer  
S.T.P. - STUDIES TECHNOLOGIES PROJECTS S.r.l. – Rome, Italy



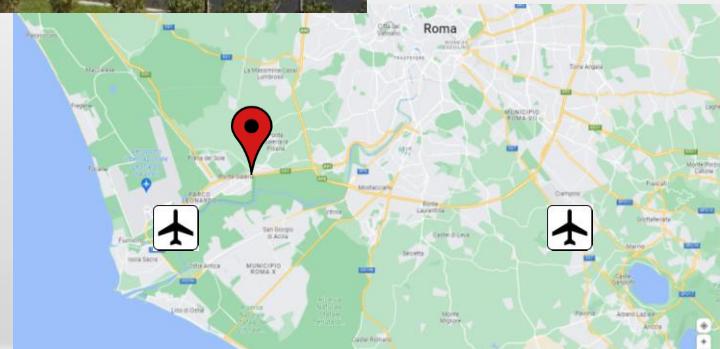
## HOME OFFICE

### Da Vinci Executive Center

Viale Alexandre Gustave Eiffel 13/15 00144 – Rome, Italy

Tel. +39-06-526257 - Fax. +39-06-52201078

E-mail: [stp@stpitaly.eu](mailto:stp@stpitaly.eu) - Web Site: [www.stpitaly.eu](http://www.stpitaly.eu)



## Thank you for your attention