

**Studi Tecnologie Progetti S.p.A.** *Engineering & Contractor* 





# USED LUBE OIL REREFINING A SUCCESSFUL INVESTMENT

Studi Tecnologie Progetti S.p.A.

Engineering & Contractor Piazzale Ezio Tarantelli, 97 Rome (Italy) www.stpitaly.eu



### **USED LUBE OIL REREFINING**



Used lube oil is a mixture of different types and grades of used lubricants, various contaminants and degradation products coming from motor crankcases and industry users.

Used Lube Oil is classified as toxic and hazardous waste to be properly disposed according to Waste Framework Directive 2008/98/EC and subject to the following requirements:

- Used Lube Oil shall be segregated and collected, not allowed to be dumped.
- Used Lube Oil shall be treated in accordance with waste hierarchy and protection of the environment and human health.
- Used Lube Oil treatments are established according to the level of contamination.



# 2 / OF USED LUBE OIL GIVE 1,5 / OF RE-REFINED OIL





Re-refining of used lube oil is an economically attractive recycling method in terms of resources conservation and environment protection. It allows processing hazardous and toxic material in a safe and effective way to recover a high quality oil product.

Used lube oil can be re-refined as many time as you like.

Used lube oil re-refining is a Circular Economy model and an attractive business opportunity as well as an environment protection process.



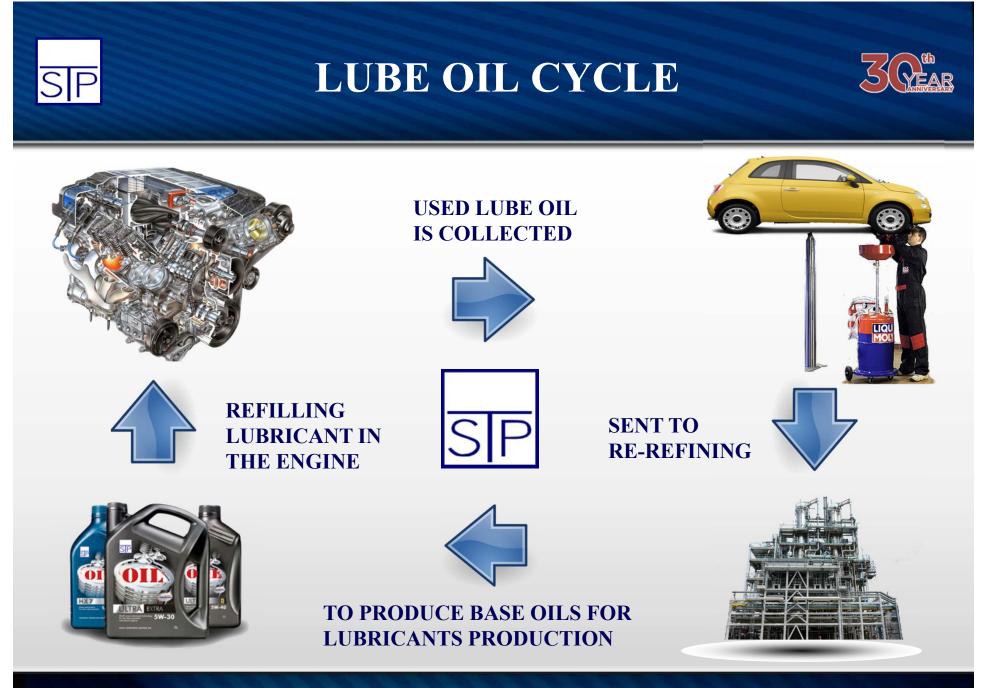
# USED LUBE OIL REREFINING CIRCULAR ECONOMY

USED LUBE OIL COLLECTION

LUBE OIL UTILIZATION

#### USED LUBE OIL RE-REFINING

**LUBE OIL PRODUCTION** 





# USED LUBE OIL RE-REFINING ADVANTAGES





# **USED LUBE OIL COLLECTION**



USED OI

USED OIL

Collection of used lube oil is the starting point for a succesfull Re-refining.

Re-refining depends on collection effectiveness and used lube oil availability.

Used lube oil is collected at garages, maintenance shops, transportation companies and industries

Efficient collection facilities are a necessity for Re-refining in terms of used lube oil quantity and quality

#### SUCCESS OF RE-REFINING DEPENDS ON THE COLLECTION SYSTEM



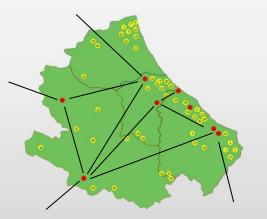


# USED LUBE OIL COLLECTION STRATEGY



- Investigation on used lube oil providers
- Division of the territory in Areas and Sectors
- Storage capacity of collection centres
- Transport network and drivers formation
- Pre-selection tests
- Segregation of contaminants

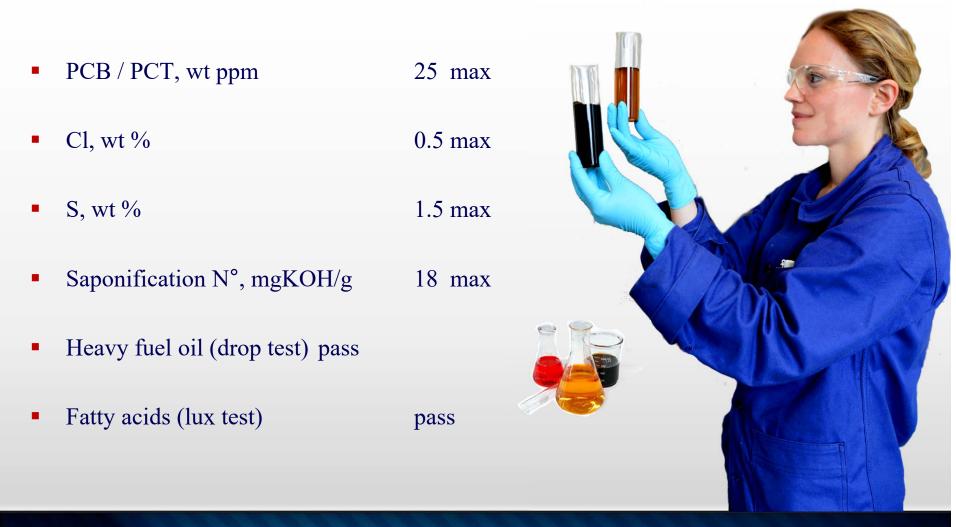




# USED LUBE OIL PRESELECTION TESTS

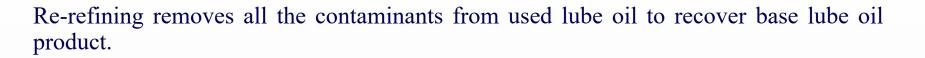
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# **USED LUBE OIL RE-REFINING**



During the last years many factors have obliged rerefiners to look for alternative Re-refining process, such as:

- increased use of additive packages in the formulation of lubricants and by consequence higher level of contaminants in the used oil
- increased amount of thermal degradation products due to longer mileage of the lubricants
- pollution problems related to the disposal of acid sludges and spent clay from the traditional acid/clay re-refining

Among the available today processes, STP Re-refining offers a low energy high yield operation, high quality products and absence of noxious wastes or by products.



STP is Pioneer on Used Lube Oil Re-refining since 30 years to produce Base oils Group I and Group II, Marine Fuel RMB-30, VGO to Oil Refinery Units.



STP has implemented several Re-refining Plants of different capacity worldwide and provide the latest high-tech green Re-refining Process.



#### USED LUBE OIL RE-REFINING PLANT STP LIST OF REFERENCES



|   | Pos. | Client                   | Location                     | Capacity TPY | Year    |  |
|---|------|--------------------------|------------------------------|--------------|---------|--|
|   | 1    | HILL GROUP               | Lithuania                    | 60,000       | Ongoing |  |
| ſ | 2    | ORIGIN INTL              | Baltimore, USA               | 160.000      | Ongoing |  |
|   | 3    | UNDISCLOSED              | Russia                       | 150,000      | Ongoing |  |
|   | 4    | AKWA                     | Mohammedia, Morocco          | 27,000       | 2017    |  |
|   | 5    | YUNITCO                  | Yanbu, Saudi Arabia          | 190,000      | 2016    |  |
|   | 6    | KLOC KSCC                | Ahmadi, Kuwait               | 33,000       | 2014    |  |
|   | 7    | VEOLIA ES                | St. Hyacinth, Canada         | 60,000       | 2013    |  |
| Ī | 8    | ECOIL Italia             | Ferrandina, Italy            | 65,000       | 2013    |  |
|   | 9    | OSILUB<br>(TOTAL/VEOLIA) | Gonfreville L'Orcher, France | 120,000      | 2012    |  |
|   | 10   | SIRAL SpA                | Nola, Italy                  | 30,000       | 2008    |  |
|   | 11   | KLOC KSCC                | Ahmadi, Kuwait               | 27,000       | 2000    |  |
|   | 12   | SOTULUB                  | Bizerte, Tunisia             | 20,000       | 1998    |  |
| ſ | 13   | GROUPO LWART             | Lençóis Paulista, Brazil     | 60,000       | 1997    |  |
|   | 14   | RAMOIL                   | Naples, Italy                | 30,000       | 1996    |  |
|   | 15   | SOTULUB                  | Bizerte, Tunisia             | 16,000       | 1989    |  |
|   | 16   | CYCLON HELLAS            | Aspropyrgos, Greece          | 25,000       | 1985    |  |

# **STP USED LUBE OIL RE-REFINING MAP**

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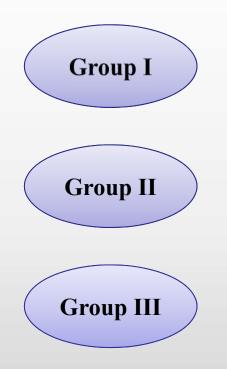




# API DEFINITION FOR BASE OILS



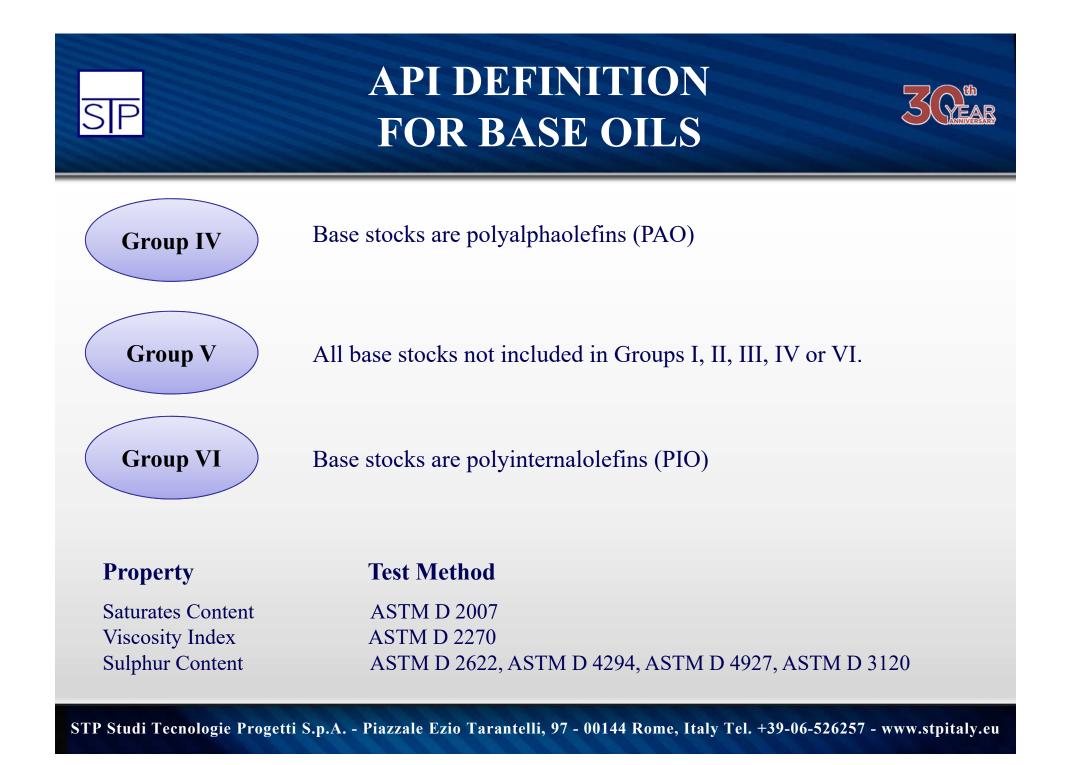
Guidelines on Base Oil Quality Assurance and Base Oil Interchange classify base stocks into six **base stock groups** according to defined physical and chemical characteristics as follows:



Base stocks containing less than 90 mass percent saturates and/or greater than 0.03 mass percent sulphur and having a viscosity index greater than or equal to 80 and less than 120.

Base stocks containing greater than or equal to 90 mass percent saturates and less than or equal to 0.03 mass percent sulphur and having a viscosity idnex greater than or equal to 80 and less than 120.

Base stocks containing greater than or equal to 90 mass percent saturates and less than or equal to 0.03 mass percent sulphur and having a viscosity index of greater than or equal to 120.





#### **STP RE-REFINING PROCESS**





STP Re-refining Process removes all the contaminants from the used lube oil and produce high quality base oil either API Group I by chemical finishing or API Group I<sup>+</sup> and Group II by Hydrofinishing.

STP Re-refining process does not release harmful or pollutant wastes to be disposed and is therefore environment friend.

Effluents are process water sent to treatment before disposal and off gas from vacuum ejector sets routed to thermal oxidizer to prevent smelling.



# **STP RE-REFINING PROCESS**



- Continuous plant operation
- High flexibility towards feedstock quality and composition
- High process yield. The lube oil recovery is more than 95% of the lubricant fraction present in the used oil.
- High separation selectivity, removal of contaminants and production of high quality base oils
- Low energy and low utility consumption
- High on-stream efficiency without corrosion, fouling, coking
- Environment safeguarding operation and no use of acid and clays
- Management of all odorous compounds to eliminate malodorous and toxic emissions
- Capital investment and operating cost highly competitive





### **UNIT OPERATIONS**



#### **1. DEHYDRATION**

Used oil is preheated to remove water, gasoline, VOC, light contaminants (solvents, glycols, lighter organic). Water is sent to treatment and lights (gasoline) are used as substitution fuel.

#### **2. GASOIL REMOVAL**

Dehydrated oil is stripped under vacuum for light gasoil removal and flash point adjustment of lube oil.

#### **3. VACUUM DISTILLATION**

Oil from gasoil stripper is sent to vacuum distillation to recover vacuum distillate oil fraction from heavier contaminants.

Vacuum distillation is carried out under high vacuum conditions, high temperature and by thin film evaporator.

Thin film evaporator achieves high selectivity and oil purification from metals, heavy polymers, carbon, dust.



### FOCUS ON THIN FILM EVAPORATOR



**Thin film evaporator** is a vertical cylindrical shell enclosed in an heating jacket with an internal rotor distributing a thin layer of oil on the heated wall, by means of rotating blades.

By the action of rotor (electrically driven) high turbulence and back mixing occur in the thin layer of the oil film and product degradation at high temperature is avoided.

Main features of thin film evaporator are:

- short residence time in order of few seconds;
- high heat transfer rate through the film;
- efficient and regenerative cleaning of the contact surface

Cracking and fouling problems are avoided by keeping low residence time, low wall temperature and high flow turbulence.

Lube oil is recovered as distillate while heavy components, additives, metals and degradation products are concentrated in the bottom residue.

### FOCUS ON THIN FILM EVAPORATOR



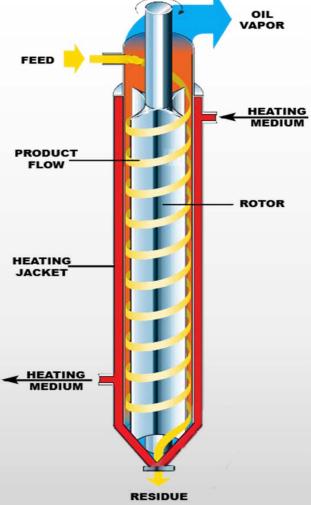
# OPERATING PRINCIPLE A Thin Film Evaporator consists of a cylindrical shell with internal rotor and external heating jacket FEED FEED

The feed is distributed by the rotor blades and spread on the heated wall to form an highly turbulent thin layer.

#### PRODUCTS

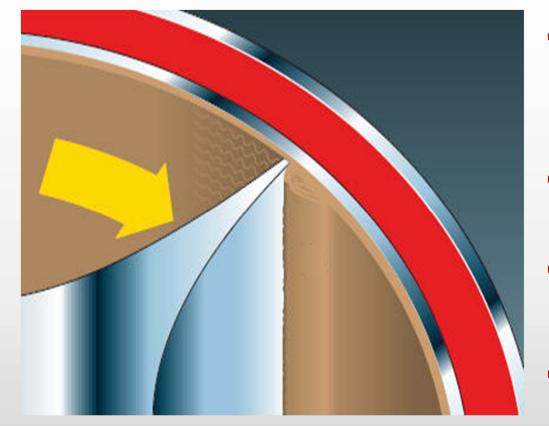
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Oil fractions are evaporated and flow out up towards the top Heavy components flow in a spiral path down to the bottom



### FOCUS ON THIN FILM EVAPORATOR





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#### **FEATURES**

- Short residence time and high turbulence in the film give high heat transfer coefficient and avoid overheating, cracking and fouling
- High evaporation rate is obtained by a simple pass
- High oil yield is achieved without degradation or polymerization of the oil
- High onstream factor and easy maintenance



### **UNIT OPERATIONS**



#### 4. FINISHING AND FINAL FRACTIONATION

Vacuum distillate is further finished to improve product quality. Finishing is done by Chemical Reactor to produce Base oil API Group I or by Hydrofinishing to produce Base oil API Group I<sup>+</sup> and API Group II. Hydrofinishing provides deep removal of contaminants such as chlorinated, sulfurous, and oxygenated organic compounds and polyaromatic hydrocarbons. Mild Hydrofinishing is used to produce Base oil API Group I<sup>+</sup>. Severe Hydrofinishing is required to produce Base oils API Group II. Finished oil is then fractionated to produce light base oil and heavy base oil.





# **STP RE-REFINING PROCESS MERITS**



- ✓ Several Used Lube Oil Re-refining Plants implemented worldwide from 16,000 Ton/year to 120,000 Ton/year capacity
- ✓ Advanced vacuum system for high vacuum level stability, based on the combined use of steam ejectors and individual tubular condensers.
- ✓ High efficiency/low pressure drops structured packing in Vacuum Distillation and Final Fractionation, to reduce pressure drops and upgrade oil yield and product separation.
- ✓ Fixed blades Thin film evaporator to avoid coking and fouling.
- ✓ Special type of API pumps and instrumentation for critical services.



# **STP RE-REFINING PROCESS MERITS**



- $\checkmark$  All pumps doubled to avoid plant shut down in case of pump failure.
- ✓ Full DCS/PLC plant automation for continuous operation.
- $\checkmark$  Indirect heating of heavy streams to prevent fouling.
- ✓ Special mechanical design for thermal flexibility, vacuum operation and fouling services.
- ✓ Use of antifouling to reduce maintenance and cleaning operation.
- ✓ Proprietary design of Base Oil Finishing for Group I, Group I<sup>+</sup> and Group II



### **PRODUCTS CHARACTERISTICS**



#### LIGHT GASOIL

Specific gravity at 15 °C End point, °C Viscosity, cst at 40 °C Sulfur, wt% Colour Flash point, °C

0.850 370 3-5 0.4 (after Hydrofinishing: 50 – 100 ppm) 2.5 (after Hydrofinishing: L 0.5) 80

Gasoil can be used as substitution fuel in the Plant or as light fuel oil in industrial fired heaters and/or boilers.

### PRODUCTS CHARACTERISTICS 3



#### MARINE FUEL RMB-30 / VGO

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| Distillation range, °C   | 370 - 550 |
|--------------------------|-----------|
| Specific gravity at 15°C | 0.900 max |
| Viscosity, cst @ 40°C    | 25-30     |
| Flash point, °C          | 210 min   |
| Sulfur, wt%              | 0.25      |
| CCR, wt%                 | 0.1 max   |
| TAN, mgKOH/g             | 0.1 max   |
| Ashes, wt%               | 0.2       |
| Metals content, wt ppm   | L 10      |
|                          |           |

VGO is used as feedstock to FCC or HDC Units







| Characteristics           | Light Base Oil       |           | Heavy Base           | Heavy Base Oil |  |
|---------------------------|----------------------|-----------|----------------------|----------------|--|
|                           | Mild                 | Chemical  | Mild                 | Chemical       |  |
|                           | Hydrofinish          | Treatment | Hydrofinish          | Treatment      |  |
|                           | Group I <sup>+</sup> | Group I   | Group I <sup>+</sup> | Group I        |  |
| Specific gravity at 15 °C | 0.870                | 0.870     | 0.885                | 0.885          |  |
| Viscosity, cst at 40 °C   | 25-32                | 25-32     | 85-95                | 85-95          |  |
| Sulfur, wt%               | 0.05                 | 0.25      | 0.05                 | 0.30           |  |
| CCR, wt%                  | L 0.01               | 0.05      | L 0.01               | 0.07           |  |
| Colour                    | L 1.0                | 2.0       | L 1.5                | 2.5            |  |
| TAN, mg KOH/g             | L 0.01               | 0.03      | L 0.01               | 0.05           |  |
| Flash point, °C           | 220                  | 220       | 260                  | 260            |  |
| Pour point, °C            | -3                   | -3        | -6                   | -6             |  |
| Metals, ppm               | absent               | L 10      | absent               | L 10           |  |





#### **API GROUP II**

| Characteristics           | Light Base<br>Oil | Heavy Base<br>Oil |
|---------------------------|-------------------|-------------------|
|                           | 0.11              | 0.11              |
| Specific gravity at 15 °C | 0.870             | 0.880             |
| Viscosity, cst at 40 °C   | 25-32             | 85-95             |
| Viscosity Index           | 110               | 115               |
| Sulfur, wt%               | L 0.03            | L 0.03            |
| Saturates, wt%            | ≥90               | ≥90               |
| CCR, wt%                  | L 0.01            | L 0.01            |
| Colour                    | L 0.5             | L 1.0             |
| TAN, mg KOH/g             | L 0.01            | L 0.01            |
| Flash point, °C           | 220               | 260               |
| Pour point, °C            | -6                | -9                |
| Metals, ppm               | absent            | absent            |
|                           |                   |                   |





| Characteristics        | Light Base | Heavy Base |         |
|------------------------|------------|------------|---------|
|                        | Oil        | Oil        |         |
|                        |            |            |         |
| PCB, wt ppm            | L 1        | L1 💡       |         |
| PCT, wt ppm            | L 5        | L 5        | o       |
| PNA, wt ppm            | L 1000     | L 1000     |         |
| Cl, wt ppm             | L 1        | L1         |         |
| Cu corrosion           | 1a         | la la      |         |
| Noack, %wt             | 10         | L 5        | · • • • |
| Saponification N°      | L 0.5      | L 0.5      |         |
| Demulsification N°     | 10         | 10         |         |
| Oxydation stability    |            |            |         |
| CCR increase, %        | 0.10       | 0.15       |         |
| Viscosity ratio @ 40°C | 2 1.09     | 1.1        |         |
| Color stability        | 1.0        | 1.0        |         |
|                        |            |            |         |

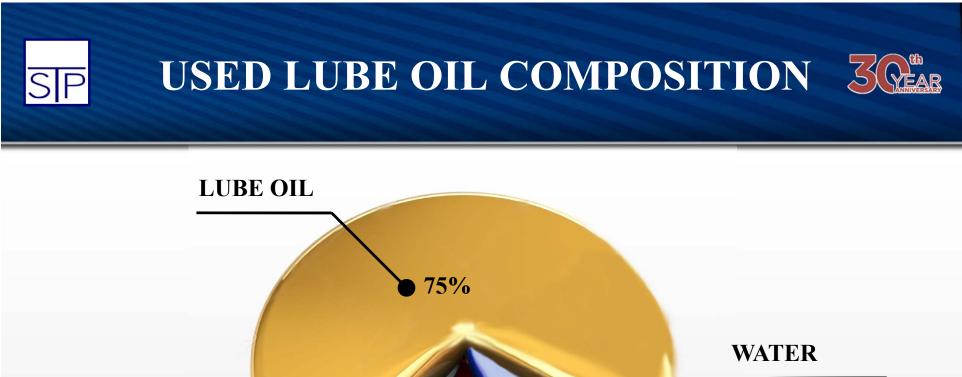






| Specific gravity at 15 °C                                    | 0.950 - 1.050       |  |
|--|---------------------|--|
| Viscosity, cst<br>at 40 °C<br>at 100 °C<br>Sulfated ash, wt% | 10,000<br>80<br>3-4 |  |
| Sulfur, wt%  | 1-2                 |  |
| Penetration, mm/10 at 25 °C                                  | 200-400             |  |
| Softening point, °C  | 15-20               |  |

Residue contains high quantity of polymers and metals and can be used for asphalt blending, production of paving asphalt, bitumen protective covering or as fuel in the cement factories.







STP Studi Tecnologie Progetti S.p.A. - Piazzale Ezio Tarantelli, 97 - 00144 Rome, Italy Tel. +39-06-526257 - www.stpitaly.eu

3%

5%

LIGHT GASOIL

7%

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# UTILITIES SYSTEMS & OFFSITE FACILITIES TO RE-REFINING



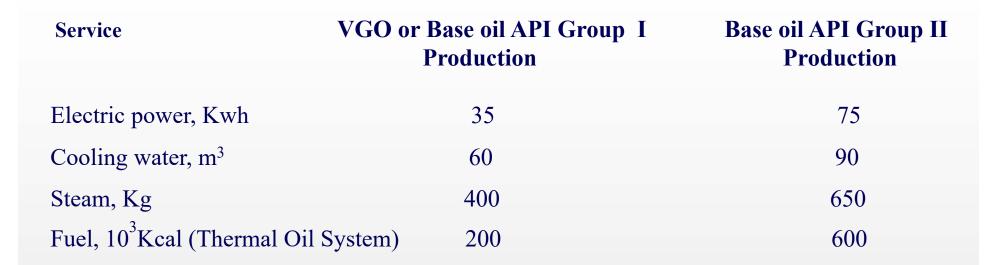
- Electric power system
- Steam system
- Cooling water system
- Compressed air system
- Sour Water Stripper
- Waste Water Treatment
- Thermal Oil System

- Thermal Oil System
- Thermal Oxidizer
- Hydrogen Plant (in case of Group I<sup>+</sup>, II)
- Fire fighting system
- Flare system (in case of Group I<sup>+</sup>, II)
- Used oil and Products storage and loading system





# UTILITIES CONSUMPTION (PER MT OF USED LUBE OIL)





## **OPERATION STAFF**



Operating labour requirements is depending on Plant operating philosophy, site location, Plant implementation within an existing complex.

Typical labor and technical staff requirement of the Re-refining Unit is as follows:

| •   | Total     | 20 | a guideline<br>preliminar |
|---|-----------|----|---------------------------|
| <ul> <li>Laboratory</li> </ul>              |           | 2  | The staffir               |
| • Workers                                   |           | 4  |                           |
| <ul> <li>Supervisors</li> </ul>             |           | 1  |                           |
| Maintenance/Workshop                        |           |    |                           |
| <ul> <li>Operators (2 per shift)</li> </ul> |           | 8  |                           |
| • Supervisor/Board person (1 p              | er shift) | 4  |                           |
| Plant Operation:                            |           |    |                           |
| <ul> <li>Plant Manager</li> </ul>           |           | 1  |                           |
|   |           |    |                           |



The staffing estimate is provided as a guideline and is intended for preliminary assessment.



### LAND AREA REQUIREMENT



The Used Oil Re-refining Unit is a very compact facility.

Typical layout area required for a 50,000 MTPY Re-refining Unit ISBL is as follows :

Production of Base Oil API Group I (without Hydrofinishing)

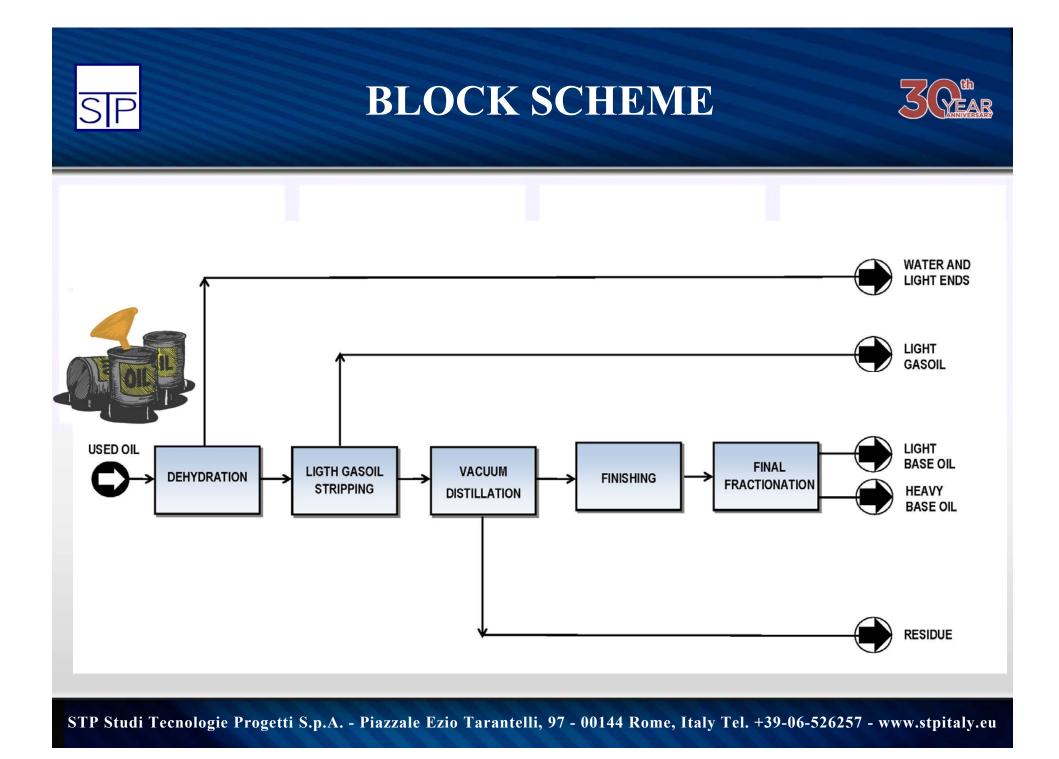
Production of Base Oil API Group I<sup>+</sup> and II (with Hydrofinishing)

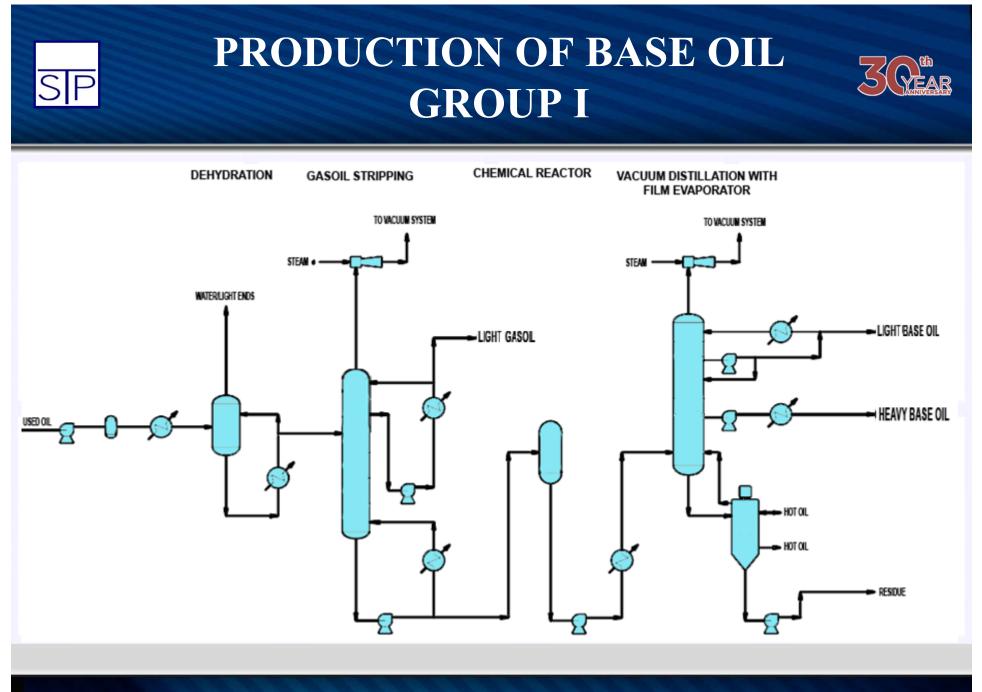




# **FLOW SCHEMES**

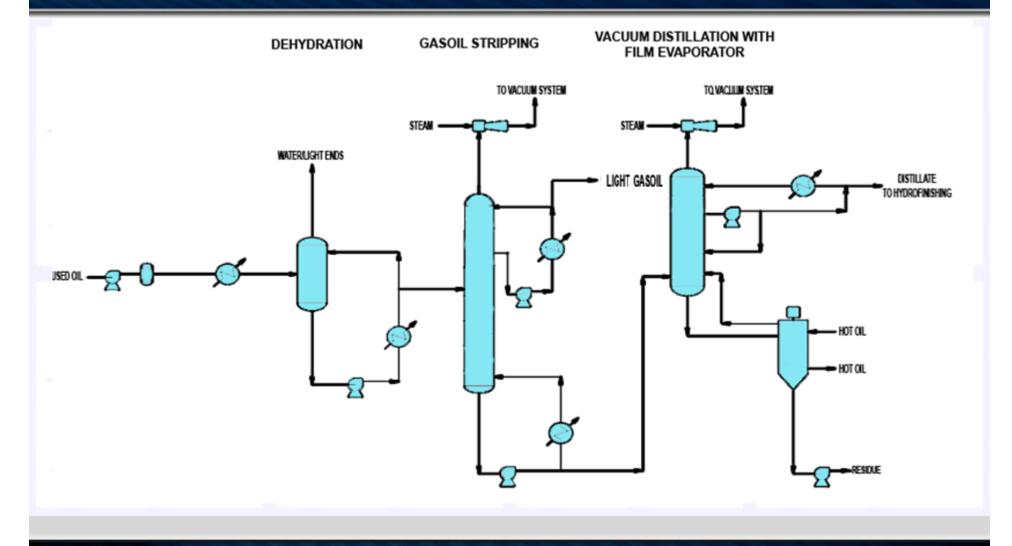


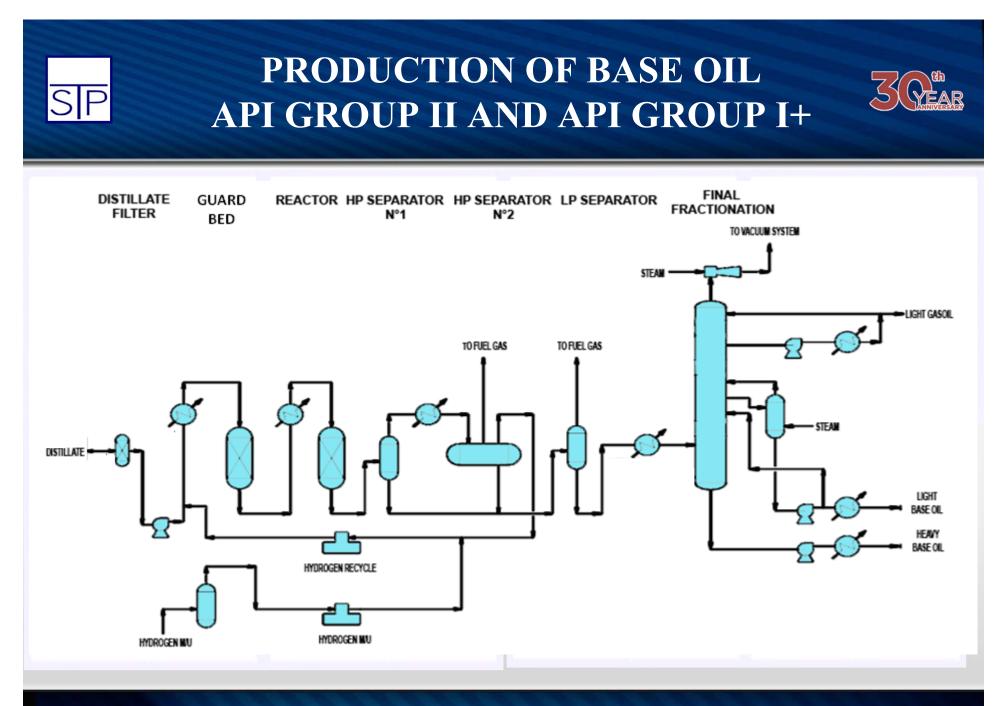




## PRODUCTION OF BASE OIL API GROUP II AND API GROUP I+

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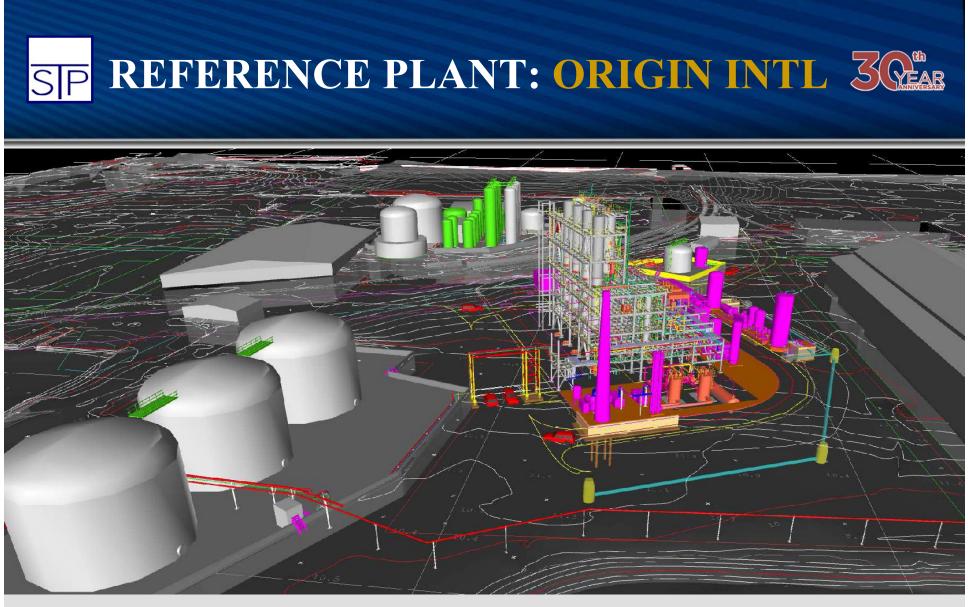




Client: HILL GROUP Klaipeda, Lithuania

Capacity: 60,000 Ton/year

**Year: Ongoing** 

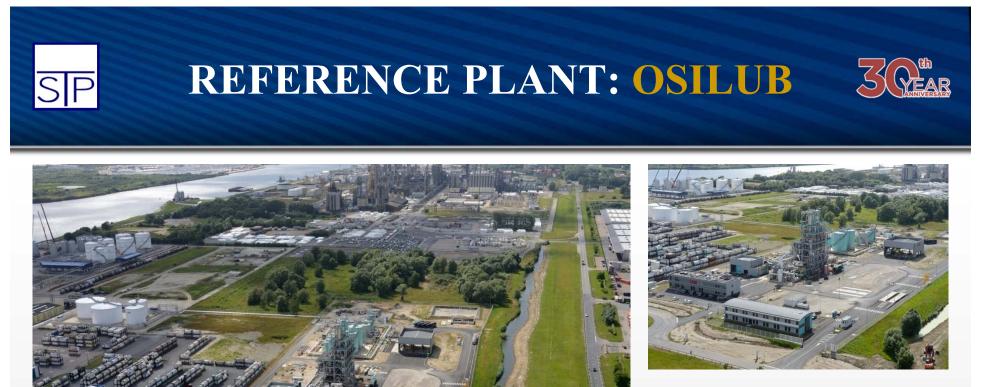


Client: ORIGIN INTL Baltimore, USA Capacity: 160,000 Ton/year

**Year: 2020** 



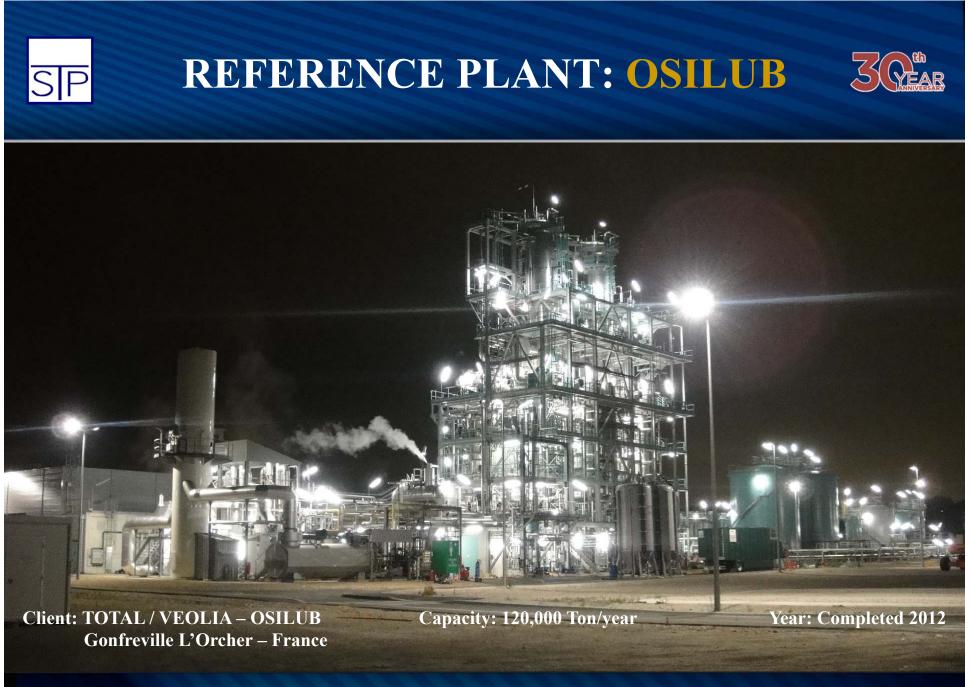






**Client:** TOTAL / VEOLIA – OSILUB Gonfreville L'Orcher – France Capacity: 120,000 Ton/year

**Year:** Completed 2012





## **REFERENCE PLANT: VEOLIA**





Client: VEOLIA ES CANADA St. Hyacinthe, Quebec **Capacity:** 60,000 Ton/year

Year: Completed 2013



## **REFERENCE PLANT: VEOLIA**



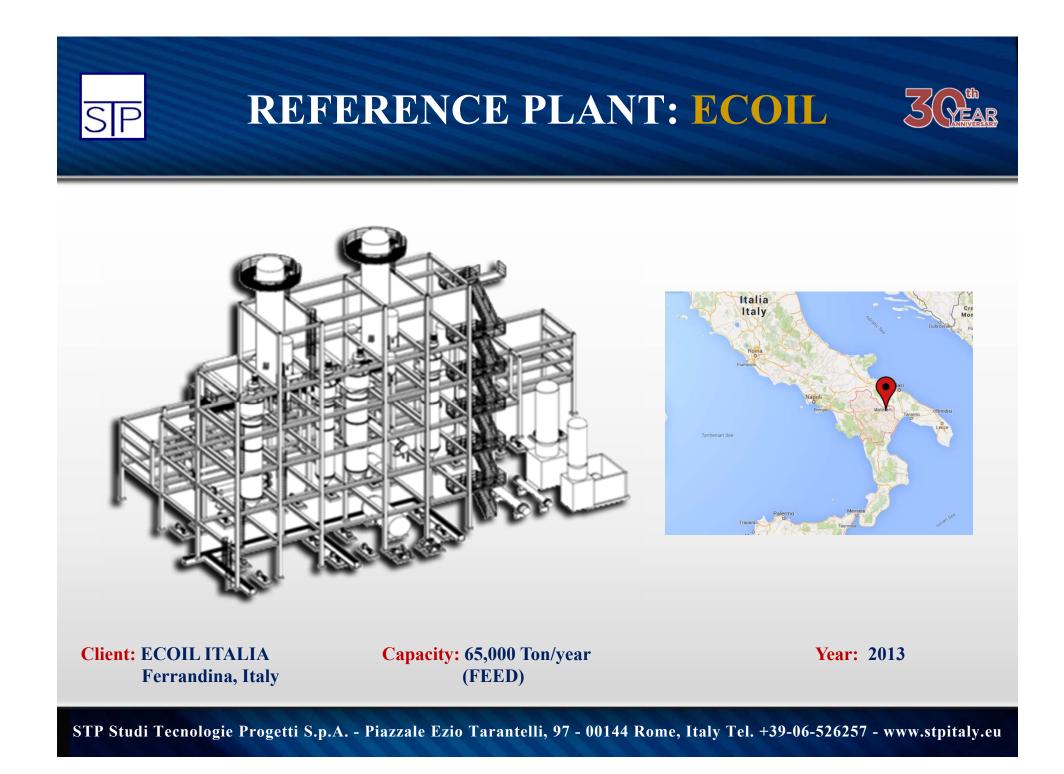


Client: VEOLIA ES CANADA St. Hyacinthe, Quebec

**Capacity:** 60,000 Ton/year

Year: Completed 2013

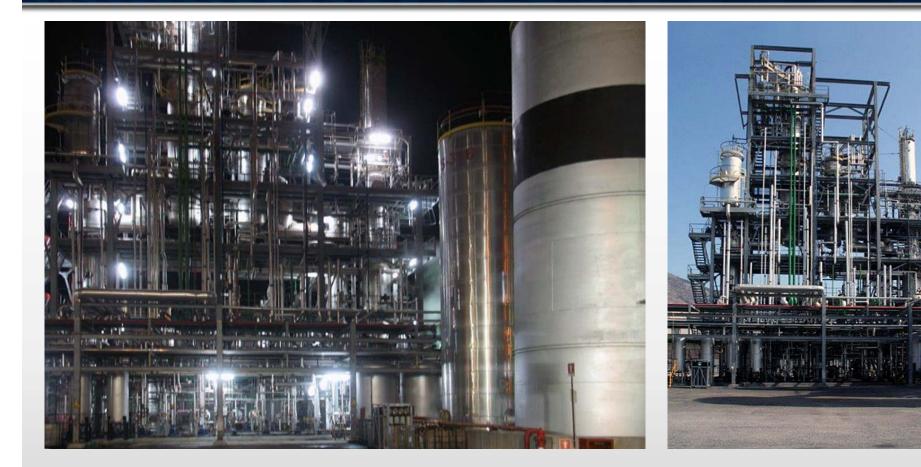






### **REFERENCE PLANT: SIRAL**





Client: SIRAL SpA Nola, Italy **Capacity: 30,000 ton/year** 

Year: Completed 2007



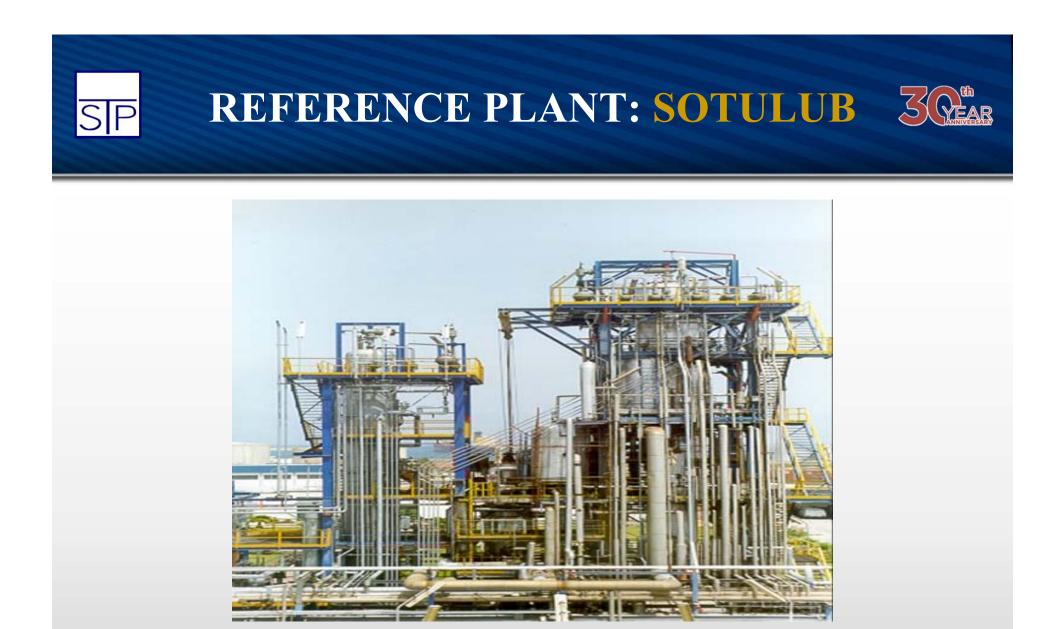
## **REFERENCE PLANT: KLOC**





Client: KLOC Kuwait Lube Oil Company Ahmadi, Kuwait Capacity: 27,000 Ton/year

Year: Completed 2000



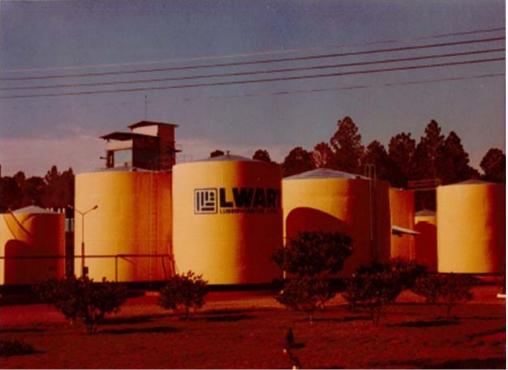
**Client:** SOTULUB Société Tunisienne de Lubrifiants Bizerte, Tunisia

Capacity: 20,000 Ton/year

Year: Completed 1999







Client: GRUPO LWART Lencois Paulista, Brazil Capacity: 60,000 Ton/year

Year: Completed 1998





Client: RAMOIL Naples, Italy

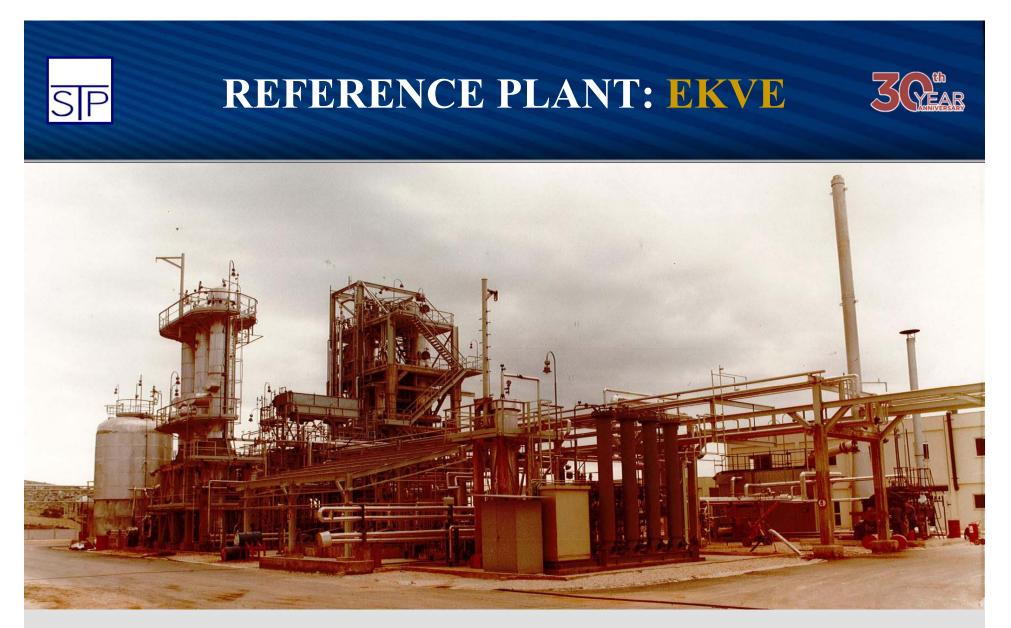
**Capacity: 30,000** Ton/year

Year: Completed 1996





Client: SOTULUB Société Tunisienne de Lubrifiants Capacity: 16,000 Ton/year Year: Completed 1989 Bizerte Tunisie



Client: CYCLON Hellas Aspropyrgos, Greece Capacity: 25,000 Ton/year

**Year:** Completed 1985



## **STP PUBLICATIONS**



### **STP Publications and Conference presentations on Used Lube Oil Re-refining:**

- □ A Project case: the 120,000 Ton/year OSILUB Re-refining Plant, 3<sup>rd</sup> CIS Base Oils, Lubrificants & Fuels Annual Conference, Moscow, Russia, May 2015.
- □ A successful waste management investment, UNEP-BIMTECH International Expert's Workshop on Destruction Technologies for Waste Oils, New Delhi, India, November 2011.
- □ A re-refining eco-friendly technology, Indian Institute of Petroleum (IIP) Workshop on Used Oil Recycling, Dehradun, India, November 1999.
- □ *Modification of existing re-refining units and realization of new modular units*, NORA Conference and Trade Show, Palm Springs, USA, November 1999
- □ *The hidden asset,* Fifth Conference on Spent Lube Oil Re-refining, Las Vegas, USA, September 1982.
- □ The used lube oil: a resource not to underevaluate, Chemical Industries Magazine, Italy, February 1982.



# **TESTIMONIALS**

## US PRESS RELEASE ON ORIGIN INTERNATIONAL OIL RECYCLING PLANT

#### **ORIGIN INTERNATIONAL INC COMMENCES BALTIMORE RECYCLING PLANT PROJECT**

#### October 28, 2019 09:03 AM Eastern Daylight Time

BALTIMORE--(BUSINESS WIRE)--Origin International Inc ("Origin") is proceeding with the next phase of development for the United States East Coast's largest and only water bounded used oil recycling plant.

CONTACTS

**Business**Wire



Rachel Deaver Public Relations 443-573-1042 rd@originamericas.us Origin is a leading environmental infrastructure and services group operating in the United States and Europe. To date Origin has established itself as one of the largest privately held used oil collectors in the United States as well as the largest mobile hydrocarbon recovery service provider in Europe which includes degassing, filtration and vapor recovery for maritime vessels, tank farms and industrial facilities.

Origin's planned construction project in its Baltimore terminal will provide the United States East Coast with its largest, most versatile and only water bounded used oil recycling plant, regenerating close to one million barrels per annum of used and contaminated liquid hydrocarbons that it can receive by truck, rail, vessel or barge. The new plant will create an estimated 200 jobs during peak construction and 20 new full-time jobs at the site, with recruitment focused on residents in the Baltimore area.

The engineering and construction management team is making progress on several fronts. Day & Zimmermann Process & Industrial division is providing overall project management services as well as engineering and procurement for offsites and utilities equipment. WBCM Construction Services with sister company Whitney Bailey Cox & Magnani LLC is performing overall construction management, preconstruction planning and permitting services. Studi Tecnologie Progetti S.p.A. Italy (STP) is performing process unit engineering, detailed design, procurement and site supervision. Becht Engineering is serving as owner's engineer for the entire project. Front-end engineering and design has been completed by STP for the process unit and is in progress for offsites and utilities. Detailed design, preconstruction site planning and permitting are underway.

"This project represents a major milestone in Origin's strategic growth plan in terms of vertical integration as well as providing a cradle to grave solution for the broadest range of waste liquid hydrocarbons. Our goal is that this plant will provide significant environmental and community related benefits to the city of Baltimore and surrounding mid-Atlantic regions," said Nicholas Myerson, CEO of Origin.

"Day & Zimmermann is excited to be part of Origin's strategic growth plan," says Bill Wasilewski, President of Day & Zimmermann's Process & Industrial Division. "We are particularly pleased to work within the capital project delivery team that has a common focus on delivering an asset that maximizes its return to investors."

#### About Origin International

Origin International seeks to acquire and consolidate strategically located oil terminals, oil processing facilities, and storage assets throughout North America and Europe. The firm's acquisition strategy focuses on waste oil recovery and recycling segments. For more information about Origin, visit <u>www.origin-international.us.</u> For more information on Origin's largest shareholder, Element Group SA, visit <u>www.element-alpha.com</u>.







CIS BASE OILS, LUBRICANTS & FUELS III Annual Conference

26-28 May 2015 Moscow, Russia

### **13:30 III USED OILS RE-REFINING TECHNOLOGIES**

•Overview of used oils collection and re-refining projects in Russia and the CIS

VLADIMIR SPIRKIN, Professor, Academician, GUBKIN RUSSIAN STATE UNIVERSITY OF OIL AND GAS

•Used oil and oil sludge recycling

**BORISS NIGROVSKY**, Sales Manager CIS, FLUID SOLUTIONS

•Waste oil treatment. A question of strategy

LUIS BERTRAND, Vice President, SWEET GAZOIL

•STP project in France: The OSILUB plant is one of the largest re-refining plant in the world CARLO GUSTAVO LOMBARDI, CEO / Managing Director, S.T.P. STUDI TECNOLOGIE PROGETTI



## PARTICIPATION TO UNITED NATIONS ENVIROMENT PROGRAMME





Our sef: 65

11 November 2011

Dear Mr. Lombardi,

I am pleased to advise that UNEP's International Environmental Technology Centre has undertaken a project to develop a Compandium of Destruction Technologies for waste oils. The compandium will include both technologies for waste oil recycling as well as destruction technologies for nen-necyclable oils through converting it into fuel and/or incinerating it. The objective is to assist developing commisse with information on destruction methologies and to earble form to assess different technologies in order to select the one unitable for their local conditions.

We are working with Birls Institute of Management and Technology, India, on this project. Apart from the Comparison of the composition of the comparison of the instructive software with some be ready selection process. A draft remain of the comparison and the instructive software will some be ready

In order to enrich the work with the knowledge and inputs from international experts, we are organizing an international Experts Workshop in New Dollai, India, from 30 November to 2 December 2011. Noting your expertite and experience in the field of works numagement, we would like to invite you as an expert to the workshop and request you to provide your valuable inputs. Please confirm your attendance to Mr. Surya Prakash Chandak, Senior Programme Officer, Email: surya chandel@inputs.org with copy to Mr. Kanuto Uwan, Programme Assistant, Email: kanka waran@inputs.org.

The detailed agends of the Workshop is attached. The verme of the workshop will be Hotel Clarion Collection (formarly Quitb Hotel) Unit of Edsepark Hotels Prt. Ltd. Shaheed Jest Singh Marg. New Delhi 110016. Upon receiving your confirmation, we will send you the draft compendium which will be discussed in the meeting.

In the light of STP's status as a large multinational company, we look forward to your early confirmation and participation in the workshop.

Sincerely yours,

Matth Director

Mr. Carlo Gustavo Londoardi CEO/Managing Diractor STP Studi Tecuologie Progetti S.r.l. Piazzale Enio Tarantelli, 97 00144 - Rome, Italy E-mail: colcombarth/a tipitaly.on

Attachment: Agenda of the workshop

Division of Technology, Industry and Economics International Environmental Technology Centre (IETC) 2-110, Ryckardi kom, Tanani-ka, Cada 3384006, Ispan, Tel +816.66915.481; Par. +81.66915.0304 E-anti-intaganag-ag, URL: http://www.ung.org/par.481.66915.0304

### UNEP - INTERNATIONAL EXPERT'S WORKSHOP, NEW DELHI - INDIA



UNITED NATIONS ENVIRONMENT PROGRAMME UNEP-DTIE-IETC

> In collaboration with Birla Institute of Management Technology (BIMTECH)

### International Experts' Workshop on Destruction Technologies for Waste Oils

### **Certificate** of **Participation**

This is to certify that Mr./Ms. Corla Gustavo Lombarde has

participated in International Workshop of experts for reviewing the draft manuscript of "Destruction Technologies for Waste Oils" held in New Delhi – India, during 30th Nov. 2011 to 2nd December 2011 in India, and has contributed in modifying the document. The workshop was organized by the United Nations Environment Programme UNEP-DTIE-IETC in collaboration with Birla Institute of Management Technology, Greater Noida – India.

Dr. H. Chaturvedi Director, BIMTECH

UNEP



### STP ATTENDANCE TO NORA CONFERENCE AT PALM SPRINGS (USA)





### National Oil Recyclers Association

12429 Cedar Road • Suite 26 • Cleveland, Ohio 44106-3172 • (216)791-7316 • Fax (216)791-6047 Kathryn McWilliams - Executive Director E-Mail Address: NatOilRA@aol.com www.noraoil.com

February 7, 2000

Carlo Lombardi STP Studi Tecnici Procedure Via D Snasotta 100 Rome, Italy 00147

Dear Lombardi:

The National Oil Recyclers Association's 1999 Conference and Trade Show in Palm Springs was a success in part because of fine presentations such as yours. Each Conference we orchestrate is built on the efforts of many individuals and I'd like you to know that your contribution was appreciated.

The Conference was well attended with over 300 people taking part in the meetings, presentations and activities. And, indications are that your presentation was received quite well.

On behalf of the Conference Planning Committee, the attendees and myself, thank you for your participation. We hope you had an enjoyable experience and trust you will consider submitting a presentation proposal for the 2000 Conference.

Sincerely

West S. Maran

Teresa S. Molnar Program Coordinator

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1999 LIQUID RECYCLING CONFERENCE AND TRADE SHOW PALM SPRINGS – November 10 – 13, 1999

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#### MODIFICATION OF EXISTING REREFINING UNITS AND REALIZATION OF NEW MODULAR UNITS

Mr. Carlo G. Lombardi Chief Executive Officer S.T.P. - STUDIES TECHNOLOGIES PROJECTS S.r.I.– Rome, Italy





# Thank you for your attention